

SECOND AND THIRD QUARTERLY REPORTS

COMBINED

# LOW TEMPERATURE BATTERY

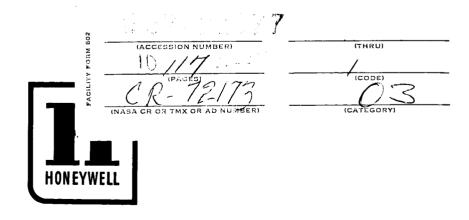
by

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prepared for

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

CONTRACT NAS 3-8503



LIVINGSTON ELECTRONIC LABORATORY

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## SECOND AND THIRD QUARTERLY REPORTS

(Combined)

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#### LOW TEMPERATURE BATTERY

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#### ABSTRACT

The system, Mg/KSCN-NH<sub>3</sub>/HgSO<sub>4</sub>:S, has been studied in both prismatic and bobbin type cells for the purpose of achieving 72 hour operation over a temperature range of +20° to -90°C. A discharge cycle of 0.3 watts for 54 minutes and 1.5 watts for 6 minutes is required for each hour.

This 72 hour goal has been exceeded at -90°C in both cell configurations with HgSO<sub>4</sub>:S:C and with S:C cathodes. A prismatic cell with a S:C cathode also performed well at -63°C. In the bobbin structure, both types of cathodes exhibited the capability of satisfactory performance throughout a temperature range of -40° to -90°C. However, the formulation containing HgSO<sub>4</sub> was much superior to the one having only sulfur and carbon.

The design of a self-contained cell in full hardware was approved. Such a cell was built and tested. Its performance at -73°C was satisfactory.

#### SUMMARY

The purpose of this program is to develop a self-contained, low temperature cell, excluding activator, based upon the battery system Mg/KSCN-NH<sub>3</sub>/HgSO<sub>4</sub>:S. It shall have the capability of operating for at least 72 hours with an alternating hourly discharge cycle of 0.3 watts for 54 minutes and 1.5 watts for 6 minutes. The desired discharge temperature range is +20°C to -90°C. An extensive investigation of the system was carried out initially at -90°C in conventional prismatic cells, followed by the construction and testing of special cells to aid in the transition from prismatic to bobbin structures. The next step was the development of a practical bobbin configuration in which the performance of the system could be studied and perfected. After satisfactory operation has been achieved, full hardware was designed and evaluated.

#### Prismatic Cell Experiments

Separation: No. M-1365 Webril paper was used in multiple layers (0.004 inches/layer). Five layers (0.020") were found to be sufficient, as demonstrated by a cell that ran for 93 hours at -90°C to 1.3 volts.

Electrolyte Studies: Thirty-four (34) weight percent KSCN in liquid ammonia is a satisfactory electrolyte for use at -90°C and has been adopted for use over the entire temperature range.

A number of salts were examined for solubility and freezing characteristics in liquid ammonia at -87°C. Sodium and lithium perchlorates, fluoroborates and hexafluorophosphates may warrant further studies.

Cathode Collector Grid Materials: Silver-plated copper Exmet is satisfactory for use at -90°C, but the plating was corroded severely at temperatures of -63° and -40°. Gold-plated copper Exmet or aluminum Exmet is recommended for use in this type of cell, especially at the higher temperatures.

Cathode Composition: Numerous combinations of components, including HgSO<sub>4</sub>, sulfur, graphite, acetylene black and paper pulp, were tested in prismatic cells. The best compostion on the average for discharge at -90°C appeared to be that containing 70 percent sulfur and 30 percent graphite.

Cathode Plate Thickness: The thickness of the cathodes ranged from 1/16 to 5/8 of an inch with the resistive load prorated accordingly. A thickness of 1/8 inch produced the best results.

Transition from Prismatic to Bobbin Cell Structures: Since the geometry of a bobbin structure usually involves single-sided discharge and possibly greater cathode depths, a variety of special designs were studied, including among others:

- 1. Single-sided discharge employing only one working anode and cathode thicknesses of 1/8 and 1/4 inches.
- 2. Multiple anodes and separately loaded cathodes with all anodes stacked on one side and all cathodes on the other, rather than in the conventional alternate method of stacking.
- 3. Cells containing reference electrodes, and
- 4. A single cathode with a separately-loaded anode on each side.

A large mass of informative data was collected which indicated among other things, that the cell performance was limited by anode polarization. In the cells with triple cathodes, failure was not due to the multiplicity of cathodes, but rather to anode current density.

Resistance and capacitance measurements were made on numerous cells. Three observations were made:

- 1. The origin of the capacitance values obtained appeared to be concentrated in the anode.
- 2. The addition of HgSO<sub>4</sub> to the cathode seemed to reduce the anode polarizing film substantially.
- 3. Capacitance values decrease markedly near end of cell life.

#### Bobbin Cell Design, Construction and Testing

Preliminary Designs for Task I: The cell configuration that was evolved and adopted for the bobbin cell experiments comprised a central star-shaped anode

with ten longitudinal fins and a cylindrical cathode located between the seperator and a conductive case. The space between the fins served as an electrolyte reservoir.

Electrolyte Studies at -90°C: The use of "spent" electrolyte from discharged cells gave the longest life, but its use was discontinued in favor of 34 weight percent KSCN in liquid ammonia when the attempts to synthesize it were unsuccessful.

Cathode Compositions: No. 1. In the absence of HgSO<sub>4</sub>, the longest life at -90°C (68 hours to 1.5 volts, 76 hours to 1.3 volts) was obtained from a mixture of 50 percent sulfur, 40 percent graphite and 10 percent acetylene black.

No. 2. The addition of about 10 percent of HgSO<sub>4</sub> to the above mixture yielded excellent results, as follows:

Discharge	Hou	rs to:*
Temp. °C	1.5V	1. 3V
~90	97	110
<b>-</b> 63	158	176
-40	97	1 27

<sup>\*</sup>Under heavy load.

Task I-B: Specifications for the construction and testing of the five ammonia cells most likely to operate at -90°C for 72 hours were prepared and approved. The design was similar to that used in the preceding experimental work, and the formulation was that shown in No. 1, above since No. 2 had not yet been developed. Upon discharge, an average life of 64 hours to 1.3 volts was achieved.

Task II, Design: A self-contained ammonia cell in full hardware, excluding activator, was designed to meet the specifications of Task II-A for the purpose of building a number of such cells for test or delivery to NASA. The system, Mg/KSCN-NH<sub>3</sub>/HgSO<sub>4</sub>:S, including the design drawings and the cathode formulation (formulation No. 2), was proposed and approved.

Task III, Test and Redesign: Based upon the approved design of Task II, mockup cells were constructed and then evaluated by discharge at -73°C. The average life was 84 hours to 1.5 volts and 99 hours to 1.3 volts.

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#### 1. INTRODUCTION

The purpose of this program is to develop a low temperature cell with the capability of delivering 1.5 watts for six minutes and 0.3 watts for fifty-four minutes each hour for a minimum of 72 hours.

Task I, "Minus 90°C Study and Test," was initiated in the first quarter. The object of this phase of the work was a study and experimental investigation of methods of extending ammonia cell operation at -90°C from the one day previously achieved\* to the goal of 72 hours. During the first quarter, the scope was limited to Method I, the development of pasted-plate cathodes for use in the system, Mg/KSCN:NH<sub>3</sub>/HgSO<sub>4</sub>:S:C. As of the close of the first three months, considerable progress had been made. Of the fifty cells tested, eight HgSO<sub>4</sub>:S:C cells had performed at -90°C under cyclic loading to the 1.3 volt cut-off for periods ranging from 71 to 117 hours, while four S:C cells ran under the same conditions from 71 to 113 hours. Task I was completed during this reporting period by the following plan of attack:

- 1. Development of prismatic cells in order to establish the best conditions for long life.
- 2. Construction and testing of a group of prismatic research cells of special design to aid in the transition to bobbin-type structures. Since the latter are usually discharged from only one side of each electrode, a number of cells were designed to study the mechanism of single-sided discharge. Some comprised only one anode and one cathode, while others had multiple anodes and cathodes.
- 3. The evolution of a bobbin cell design through the application of the knowledge gained from the prismatic cell studies and from experimentation with variations in bobbin structures, methods of construction, cathode compostion and electrolyte concentration and type.

Task II, "Design," required the design of a self-contained ammonia cell, excluding activator, for the purpose of fabricating a number of such cells for test or delivery to NASA. This was accomplished during the third quarter.

<sup>\*</sup>Contract NAS 3-6009

Task III, "Test and Redesign." In the first part of this task, a full-scale cell mockup was constructed and evaluated with satisfactory results. This concluded the activities of the third quarter and placed the project in good position to complete Task III during the fourth quarter.

Supporting data for all cells are provided in Appendix A which includes:

Notes to Tables

Materials Identification

Table I - Electrochemical Cell Tests, Pasted-plate Configuration

Table II - Electrochemical Cell Tests, Bobbin Configuration

Table III-A - Periodic Cell Voltages, Pasted-plate Configuration

Table III-B - Periodic Cell Voltages, Bobbin Configuration

Cell construction, illustrations and drawings are included in Appendix B.

#### 2. PRISMATIC CELL EXPERIMENTS

The method of construction and a drawing of a typical prismatic (or pasted-plate) cell may be found in Appendix B. The test results are discussed in the following sections.

#### 2.1. Separation

The effect of variations in separator thickness are shown in Table I.

TABLE I
Separation Thickness Studies

Cell No.	HgSO <sub>4</sub>	S g	C g	Electrolyte Vol. (cc)	Separator Thickness (in.)	Hours to 1.3V
51	20	4	12	150 <sup>a</sup>	0.020	70
52	20	4	12	100	0.020	93
59	20	4	12	100	0.028	26
60	20	4	12	100	0.028	56
62	0	11	11	100	0.008	64

<sup>\*</sup>Webril No. M-1365.

The increase in thickness from 20 to 28 mils was detrimental, possibly because of increased resistance. A decrease in thickness to 8 mils in a S/C cell yielded moderately good results. The optimum was not established definitely because of the limited number of tests, but the 20 mil thickness has been adopted as a suitable standard. This is made from 5 layers at 4 mils each.

<sup>\*\*</sup>Under heavy load.

<sup>&</sup>lt;sup>a</sup>100 cc initially: added 50 cc after 2 days, at which time the heavy load voltage recovered from 1.53 to 1.83.

#### 2.2. Electrolyte Studies

Twenty-five and 34 weight percent KSCN in liquid ammonia and partially "spent" electrolytes were used in a number of cells. Other variables were cathode composition, discharge temperature and collector grid materials. The results are summarized in Tables II and III.

TABLE II

Electrolyte Concentration Variations (No. 1)

Cell No.	Wt. %	Temp.	Но	urs to
<u>P-</u>	KSCN	<u>°C</u>	1.5V	<u>1.3V</u>
120	34	-40	35	51
121	34	-40	29	38
118	34	-63	32	38
119	34	-63	35	39
125	25	-63	41	43**
130	25	-63	25	30

<sup>\*</sup>Under heavy load.

Corrosion was more evident at higher temperatures; and the silver-plate was destroyed, thereby exposing the copper Exmet grid. Neither the substitution of aluminum Exmet or the use of more dilute electrolyte proved to be substantially beneficial.

<sup>\*\*</sup>Aluminum Exmet collector grid: silver-plated copper Exmet used in all other cells.

TABLE III

Electrolyte Concentration Variations (No. 2)

Electrolyte							
Cell No.	S	С	Wt. % as	KSCN	Temp.	Hou	rs to*
P-	<u>%</u>	<u></u> %_	Virgin	''Spent'' <sup>1</sup>	<u>°C</u>	1.5V	1.3V
131	70	30	25		-63	45	82**
1 32	70	30	25		-63	57	83**
1 28	70	30		25	-90	25	110
1 29	70	30		25	-90	90	113
76	70	30	34		-90	99	141
77	70	30	34		-90	100	120
1 26	85	15	25		-90	0	95
1 27	85	15	25		-90	17	89
58	85	15	34		-90	53	89

<sup>\*</sup>Under heavy load.

The S:C cells (P-131 and 132) ran at -63°C almost twice as long as P-125 (Table II) which contained  $HgSO_4$ . Aluminum Exmet grids were used in these three cells. At -90°C, P-128 and 129 ran well with "spent" electrolyte, but not nearly as long as P-76 and 77 in which 34 Wt. % KSCN was used.

The use of only 15 percent graphite in conjuction with 25 percent KSCN (cells P-126 and 127) yielded very short runs to 1.5V, but long life to 1.3V at -90°C. However, the use of 34 percent KSCN in a similar cell, P-58, provided better performance to the 1.5V cut-off.

Therefore, the results are strongly in favor of the use of 34 Wt. % KSCN in liquid ammonia as the electrolyte for pasted-plate cells having S:C cathodes.

<sup>\*\*</sup>Aluminum Exmet collector grid: silver-plated copper Exmet in all other cells.

<sup>&</sup>lt;sup>1</sup> "Spent" electrolyte is the residual electrolyte from a similar cell after discharge.

#### 2.2.2. Electrolyte Volume and Level

It has been demonstrated in Cell No. 51 (Table I), and in some latter cell tests that the volume and level of electrolyte are important factors that must be checked throughout discharge. The required quantity cannot be predicted accurately because different cathode mixtures absorb or consume different amounts of electrolyte and because the plastic envelope cell containers vary somewhat in size. If the level is above the connections of the lead wires to the electrodes, the connections are attacked and may be destroyed even if they are coated with such materials as Krylon or rubber cement. In order to eliminate this problem, longer anode and cathode collector tabs were adopted. This permits the use of a safe excess of electrolyte. If the electrolyte level is too low, the cells suffer in life span.

#### 2. 2. 3. Electrolyte Salts Other Than KSCN

It would be desirable to have available solutions of salts in liquid ammonia that would have lower freezing points and better electrical conductivities than presently obtainable with KSCN. Some preliminary experiments were made on solutions of eight salts in liquid ammonia. A sufficient weight of each salt to produce a 30 percent solution was added to ammonia at -40°C. After the maximum amount of salt had dissolved, each solution or mixture was cooled to -87°C and the behavior was noted. The observations are summarized below:

Salt	Concentration at 40°	Observations at -87°
Lithium chloroaluminate (LiAlCl <sub>4</sub> ) Potassium chromate (K <sub>2</sub> CrQ <sub>4</sub> )	Negligible Negligible	
Sodium bromide (NaBr)	30%	Solution froze.
Sodium perchlorate (NaClO <sub>4</sub> )	30%	Did not freeze completely-lower portion fluid
Lithium perchlorate (LiClO <sub>4</sub> )	30%	Did not freeze.
Lithium fluorosulfonate (LiSO <sub>3</sub> F)	30%	Solution froze.
Lithium tetrafluoroborate (LiBF <sub>4</sub> )	30%	Partial freezing- upper portion fluid.
Lithium hexafluorophosphate (LiPF <sub>6</sub> )	30%	Did not freeze.

The perchlorates showed promise but are potentially dangerous when confined

in cell hardware. The last three salts appeared to generate some gas which indicated possible instability, and only the last two did not freeze completely. It would seem, therefore, that a more thorough study of only the last two salts and others as yet untried could be justified.

#### 2.3. Cathode Collector Grid Materials

Table IV presents the comparative performance of several grid materials with changes in cathode composition and discharge temperature.

TABLE IV

Cathode Collector Grid Materials Studies

Cell No.	HgSO₄	s	С	Temp.	Collector Material (Superscripts defined in	Ave.	hrs. to
P-		%_	%	°C	Appendix A notes	1.5V	1.3V
52	55.6	11.1	33.3	-90	Ag-plated Cu Exmet <sup>w</sup>	81	93
63	55.6	11.1	33.3	-90	Ag Exmet <sup>x</sup>	5 <b>4</b>	66
130	55.6	11.1	33.3	-63	Ag-plated Cu Exmet	25	30
125	55.6	11.1	33.3	-63	Aluminum Exmet <sup>ZZ</sup>	41	43
58,70	0	85	15	-90	Ag-plated Cu Exmet <sup>w</sup>	54	87
74, 75	0	85	15	-90	Ag Exmet <sup>x</sup>	2	41
99,105	0	85	15	-63	Ag-plated Cu Exmet w	50	75
108	0	85	15	-63	Perforated Aluminum yy	0	0
109	0	85	15	-40	Perforated Aluminum <sup>yy</sup>	0	0
Typical	0	70	30	-90	Ag-plated Cu Exmet <sup>w</sup>	85	111
100 to 104	0	70	30	-63	Ag-plated Cu Exmet <sup>W</sup>	43	55
106,107	0	70	30	-63	Lead Exmet <sup>xx</sup>	40	55
110	0	70	30	-63	Perforated Aluminum yy	15	44
112,113	0	70	30	-63	Au-plated Cu Exmet <sup>ww</sup>	64	74
131, 132	0	70	30	-63	Aluminum Exmet ZZ	51	82
116,117	0	70	30	-40	Ag-plated Cu Exmet w	19	23
111	0	70	30	-40	Perforated Aluminum yy	13	37
114,115	0	70	30	-40	Au-plated Cu Exmet <sup>ww</sup>	36	45

<sup>\*</sup>Under heavy load.

It was concluded in the first quarter that silver-plated copper Exmet was a satisfactory collector grid for use at -90°C. This was formed by expanding a 20 mil sheet to yield strands 30 mills in width and small openings. Subsequent, tests were made on pure silver Exmet which was expanded from 5 mil sheet to form 8 mil strands and relatively large openings in the mesh. It is believed that the open-mesh pure silver Exmet did not function well because of poor conductivity in the cathode mixture of cells P-74 and 75, which contained only 15 percent carbon in the S/C cathodes. This is substantiated partially by the better performance of the HgSO<sub>4</sub>/S cell, No. P-63.

At higher temperatures, such as -63° and -40°, there was a general trend toward shorter cell life and increased corrosion of most grids and anodes. Gold-plated copper Exmet (Nos. P-112 to 115) was superior to the silver plate, and aluminum Exmet was also somewhat better than the silver plate (P-125 vs 130). In the latter instance, at -63° the silver was removed, possibly due in part to the presence of HgSO<sub>4</sub>. However, in cells P-116 and 117, which contained no HgSO<sub>4</sub> but which were discharged at -40°, all of the silver-plate was removed, and the copper grid was almost destroyed. Lead Exmet lasted for over two days but was found to be completely disintegrated after four days. There was no corrosion resistance of aluminum and to secure better adhesion of the paste to the grid, it was used in the form of Exmet in cells P-131 and 132. The life of 82 hours to 1.3 volts indicated it to be quite satisfactory for use at -63° with the 70:30 S/C mix.

It is concluded from the available data that either gold-plated copper or aluminum in the form of Exmet should be used in any future pasted-plate fabrication.

#### 2.4. Cathode Composition

The proportions of HgSO<sub>4</sub>, sulfur, graphite, acetylene black and paper pulp have been varied in the cathode mix. The test cells were of standard construction with silver-plated copper Exmet collector grids. The electrolyte was 34% KSCN in liquid ammonia. A number of tests from the first quarter are included to provide a more complete picture.

#### 2.4.1. HgSO<sub>4</sub>/S/Carbon Cathodes

TABLE V

Cathode Variations with Mercuric Sulfate

Cell No.	Mol ratio S:HgSO <sub>4</sub>	HgSO <sub>4</sub>	S %	C 	Temp.	Hour 1.5V	s to*
17, 22, 29, 35		0.0	41.4	58.6	-90	57	66
18, 23, 30, 36	4:1	40.8	17.7	41.5	-90	54	64
19, 28	2:1	51.5	11.2	37.3	-90	58	66
9-14, 51, 52	1.86:1	55. <b>6</b>	11.1	33.3	-90	58	66
25, 31, 37	1.1	60.0	6.4	33.6	-90	59	65
21,27	0	70.8	0.0	29.2	-90	38	41
118, 119	1.86:1	55.6	11.1	33.3	-63	34	38
120, 121	1.86:1	55.6	11.1	33.3	-40	32	45

<sup>\*</sup>Under heavy load.

At -90°c, all of the above combinations, except the one without sulfur, yielded about the same average life and had at least one cell in each group that met the three day requirement. Without sulfur, the performance was erratic and unpredictable. Reproducibility was best in the absence of HgSO<sub>4</sub>.

At the highest temperatures, -63° and -40°, corrosion of the collector grids was severe, and the performance was unsatisfactory.

It would have been desirable to have established the most effective ratio of oxidant to graphite for each combination of oxidants. An example of such a determination may be found in the next section, 2.4.2.

#### 2.4.2 Sulfur/Carbon Cathodes

TABLE VI

Cathode Variations without Mercuric Sulfate

Cell No.	S	С	Temp.	Hour	s to*
<u>P-</u>		_%_	•°C	<u>1.5V</u>	1. 3V
17, 22, 29, 35	41.4	58.6	-90	57	66
34	50.0	50.0	-90	79	85
78,79	60.0	40.0	-90	93	105
76,77,96,97	70.0	30.0	-90	85	111
33, 38, 58	85.0	15.0	-90	79	105
32	100.0	0.0	-90	0	8
100 to 104	70.0	30.0	-63	43	55
99, 105	85.0	15.0	-63	50	75
116,117	70.0	30.0	-40	19	23

<sup>\*</sup>Under heavy load.

This table and the accompanying graph, Figure 1, show the optimum composition of a S/C cathode for discharge at -90° to be about 70 percent sulfur and 30 percent graphite.

Eighty-five percent sulfur appears to be better for discharge at -63°. However, one cell (P-102) in the 70 percent S group ran for 66 hours to 1.5V and for 75 hours to 1.3V.

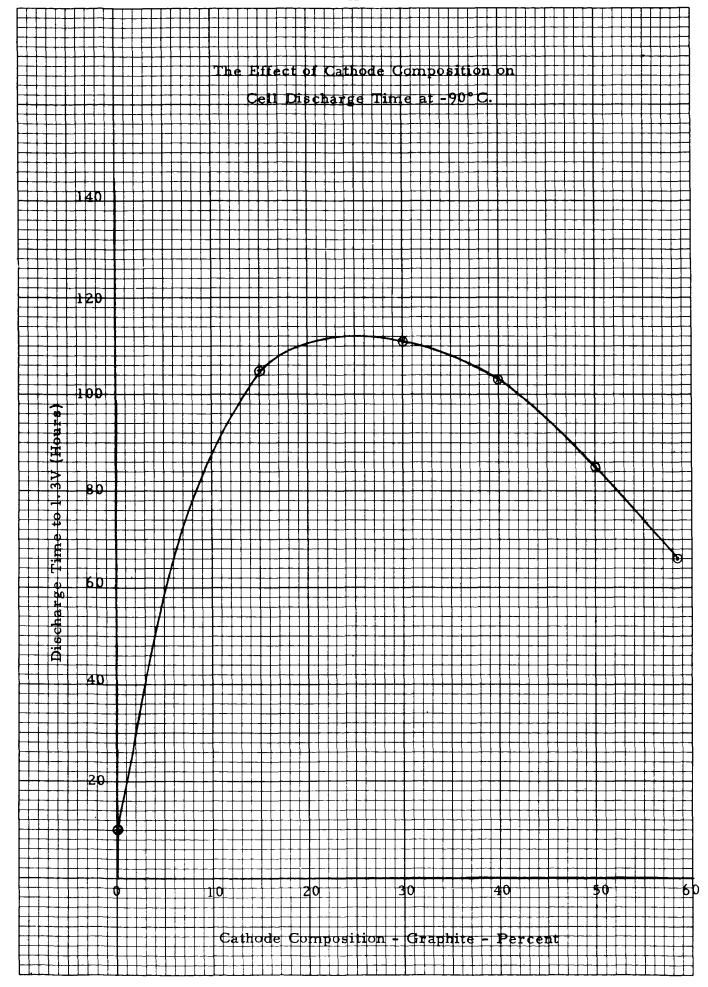


Figure 1

#### 2.4.3. Acetylene Black

In Table VII, the results of substituting acetylene black for part of the graphite are summarized. All cells were discharged at -90°C.

TABLE VII

Graphite/Acetylene Black Variations

Cell No.	S g	Graphite	Acet. Black	Total Carbon	Electrolyte Vol. (cc)	Ave. Hours* to 1.3V
76,77	17	7.3	0	30	125	130
96, 97	17	7.3	0	30	100	93
83	17	6.6	0.7	30	125	87
91	17	6.6	0.7	30	100	80
84	17	5.9	1.4	30	125	108
92	17	5.9	1.4	30	100	86
33, 38	21	3.7	0	15	100	105
58	21	3.7	. 0	15	100	105
81	21	3.3	0.4	15	125	118
89	21	3.3	0.4	15	100	72
82	21	2.9	0.8	15	125	121
90	21	2.9	0.8	15	100	85

<sup>\*</sup>Under heavy load.

Only those cells containing equal amounts of electrolyte can be compared with each other, for it is evident that this factor had a greater influence on performance than the additive. It is difficult to draw a definite conclusion from these data. Every cell, however, met or exceeded the 72-hour requirement.

#### 2.4.4. Paper Pulp

Table VIII is a summary of the test results at -90°C on cells in which paper pulp was added to the cathode composition.

TABLE VIII

#### Paper Pulp Additive

Cell No.	S g	C g	C <u>%</u>	Paper Pulp	Electrolyte Vol. (cc)	Ave. Hours* to 1.3V
76,77	17	7.3	30	0	125	130
96,97	17	7.3	30	. 0	100	93
85	17	7.3	30	0.25	100	89
86	17	7.3	30	0.75	120	109
33, 38	21	3.7	15	0	100	105
58	21	3.7	15	0	100	105
87	21	3.7	15	0.25	110	100
88	21	3.7	15	0.75	130	69

<sup>\*</sup>Under heavy load.

No advantage can be attributed to the addition of paper pulp, and it seemed to have a harmful effect, particularly on Cell No. P-88. Additional electrolyte had to be added to compensate for absorption by the pulp.

#### 2.5. Cathode Plate Thickness

The thickness of the pasted plates normally used for most of this work has been about 1/8 inch, regardless of the composition. In the experiments shown in Table IX, the thickness was varied. Since the area was constant, the cathode weights necessarily changed, and the resistive loads were adjusted accordingly. The peak anode current density varied approximately in proportion to the applied load.

TABLE IX

Positive Electrode Thickness Variations

Cell No.	Thickness in.	HgSO <sub>4</sub>	S g	C g	Loads, $\Omega$	Peak C. D. mA/cm <sup>2</sup>	Hours to*
13 cells	1/8	20	4	.12	13.5/68	0.81	117
				imum			28
			Min	imum		0.70	
			Av	erage		0.76	63
43	5/8	100	20	60	2.7/13.5	3.67	38
44	5/8	100	20	60	2.7/13.5	2.91	20
54	5/8	100	20	60	2.7/13.5	3.42	30
46	1/16 <sup>a</sup>	5	l	3	48/240	0.22	49
47	1/16, <sup>a</sup>	5	1	3	48/240	0.22	48
61	1/16 <sup>b</sup>	5.9	5 1.19	3.57	48/240	0.22	82

<sup>\*</sup>Under heavy load.

The life span of HgSO<sub>4</sub>/S cells has been highly erratic and unpredictable, and the factors affecting it have not been identified with certainty. However, these data and other observations which will be reported later indicate that anode current density is a limiting factor.

Cells P-46 and 47, in which the grids were not completely covered, ran for a relatively short time in comparison with No. P-61. This and the relation between grid corrosion and cell life, which was evident in tests at higher temperatures, lead one to the opinion that grid corrosion in some way poisons a cell.

<sup>&</sup>lt;sup>a</sup>Just enough paste to fill pores of collector grid.

bGrid surface covered somewhat better than in (a).

#### 2.6. Transition from Prismatic to Bobbin Cell Structures

A conventional prismatic or pasted-plate cell (as described and illustrated in Appendix B, pages B-l and B-2) may be comprised of a single cathode with a Mg anode on each side. Most cells were designed to provide 1/5 of the capacity required by a full-sized cell. The experiments covered in this section were conducted primarily to gain the information required for the design of a bobbin cell with the capability of satisfactory operation at -90°C.

#### 2.6.1. Single-Sided Discharge

The geometry of a bobbin cell usually involves what may be termed singlesided discharge between an anode and a cathode. This is contrasted to the multiple flat-plate structure sometimes referred to as prismatic where, with the exception of the outside plates, all electrodes are discharged from two surfaces towards the center. In single-sided discharge, one flat plate cathode may be discharged against a flat plate anode. In this case the current from the side of the cathode which is nearest the anode need not travel through the depth of the porous cathode structure. On the other hand, the electrolytic current from the cathode side facing away from the anode must pass through the pores of the complete cathode thickness. This characteristic may be a limiting factor in the operation of bobbin type cathodes. The greater cathode thickness inherent in the bobbin cell was explored in a rather unique fashion by means of a similar construction employing more than one porous cathode or anode grouped together to simulate a single thick porous cathode and anode. However, the individual plates in several cases were electrically insulated permitting the recorded data to be, in effect, stratified as to cathodic thickness. These exploratory structures were quite useful in defining some of the limiting factors of the magnesium/KSCN: NH<sub>3</sub>/S:HgSO<sub>4</sub>:carbon cell as it applies to bobbin type structures.

Not only was it possible, by this means, to determine the effect of electrode thickness upon discharge characteristics, but the location of porous reference electrodes between a working cathode and a working anode of the flat plate type permits a clear definiation from the standpoint of geometry as to which electrode is controlling the increase or decrease of cell voltage, including the effect of porous electrode thickness. The following paragraphs, 2.6.1.1. through 2.6.1.3., describe such cells and the conclusions which were drawn therefrom.

#### 2.6.1.1. Single Cathode, Single Working Anode

In the first quarter, a cell, No. B-50, was discharged at the full prorated load from one anode while the other anode was utilized as a reference. Difficulties were encountered with the reference electrode, indicating working anode cut-off.

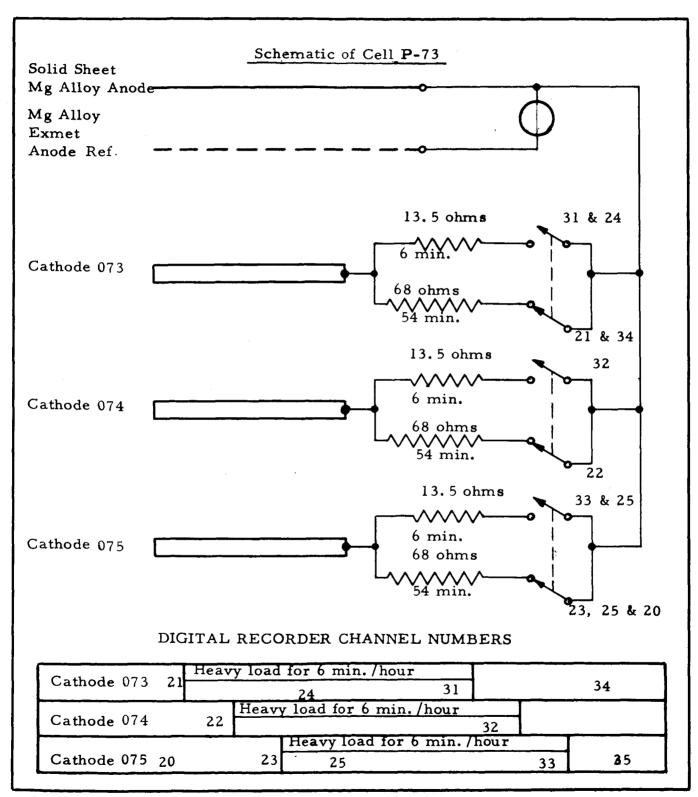
Cells P-94 and 95 were constructed with only one anode and one cathode, thereby doubling the normal anode current density. As a result, the life span was reduced drastically to an average of about 56 hours.

In a further investigation of the effect of electrode geometry, cells were constructed with cathodes on which the applied paste was localized on one side for cells P-65 and P-66, and which was 1/4" thick (double thickness) for cells P-71 and P-72. It had been expected that cell P-65, wherein the cathode mixture was loaded onto the anode side of the silver-plated cathode collector, would be superior. However, cell P-66 which was the converse of this, was decidedly better. Both cells might, of course, be considered to be limited by the effect of anode polarization at double the design center current density. The 1/4" thick cathode cells, P-71 and P-72, were discharged with single anodes, and it is presumed now in the light of additional data that the reduced service hours were due to anode polarization at four times design center current density resulting from the prorating of the load upon cathode theoretical capacity.

#### 2.6.1.2. Triple Cathodes, Single Working Anode

#### Flat-Plate Equivalent of a Bobbin Cell

Cell P-73 consisted of a flat anode, a reference Exmet anode, and three separately loaded cathodes, all on the same side of the working anode. The load current of all three cathodes was, therefore, channeled through the inside working cathode. It is interesting to note that the performance of this cell, while substantial, was limited not by the multiplicity of cathodes, but rather by anode current density. Refer to Figure 2 and Table X. For example, in Table X at 42 hours channels 31-33 show the significant effect of anode current density upon output voltage.



FORM FM-100

Figure 2

TABLE X
PERIODIC CELL VOLTAGES

#### Cell No. P-73

Elapsed										
Time	Channel Numbers									
(Hours)	21 22 23	24 25 31	32 33 34 35							
First	1.91 1.82 1.65	1.39 1.13 1.33	1.45 1.46 1.88 1.84							
6	1.56 1.11 0.80	0.66 0.54 0.67	0.86 0.95 1.61 1.53							
12	1.43 0.91 0.58	0.46 0.40 0.56	0.75 0.85 1.60 1.50							
18	1.72 1.47 1.15	0.90 0.75 0.79	0.92 1.02 1.62 1.55							
24*	1.83 1.63 1.35	1.15 1.08 1.35	1.55 1.47 1.85 1.77							
30	1.85 1.75 1.53	1.26 1.15 1.24	1.46 1.44 1.85 1.79							
36	1.82 1.57 1.27	0.97 0.86 0.95	1.22 1.29 1.83 1.75							
42	1.69 1.32 0.96	0.69 0.59 0.75	1.03 1.12 1.86 1.88							
48**	1.87 1.80 1.59	1.34 1.23 1.28	1.48 1.40 1.85 1.78							
5 <b>4</b>	1.90 1.83 1.60	1.29 1.16 1.21	1.42 1.36 1.82 1.79							
60	1.81 1.65 1.38	1.12 1.01 1.07	1.30 1.27 1.77 1.72							
66	1.79 1.61 1.32	1.04 0.95 0.99	1.22 1.21 1.75 1.68							
72	1.78 1.57 1.26	1.01 0.91 0.96	1.19 1.17 1.74 1.68							
78	1.75 1.52 1.20	0.96 0.86 0.92	1.14 1.14 1.71 1.65							

<sup>\*</sup> Switched from flat Mg to expanded Mg at 23rd hour.

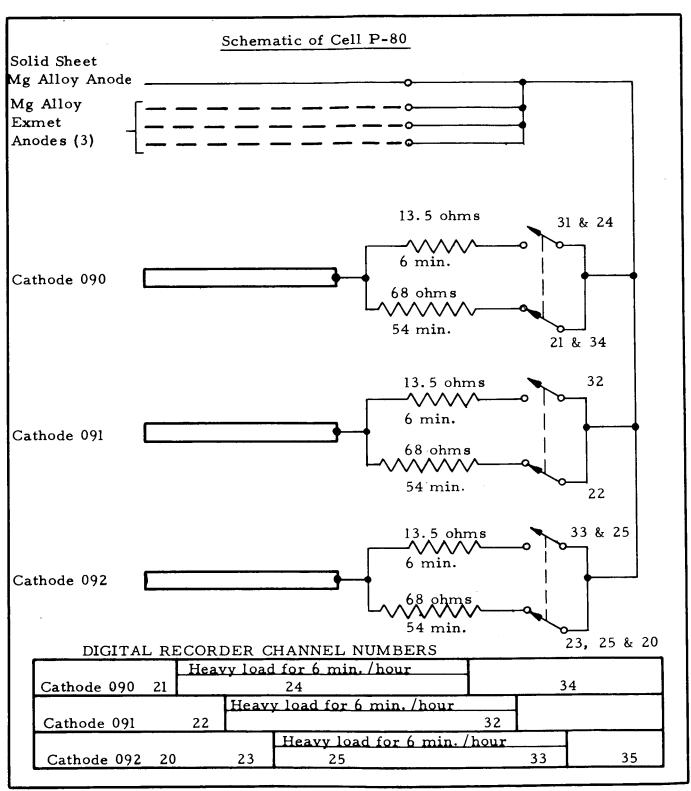
Note: Both flat and expanded Mg electrodes on one side of the three cathodes.

<sup>\*\*</sup> Discharging from both flat and expanded Mg at 43rd hour.

#### 2.6.1.3. Triple Cathodes, Multiple Anodes, Cells P-80 and 93

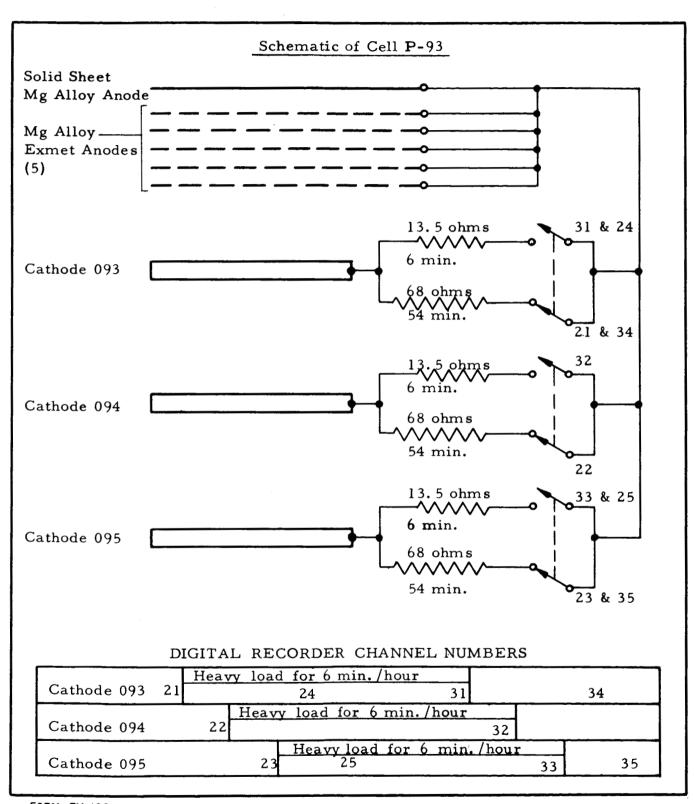
Schematic drawings of the arrangement of the multiple electrodes, the electrical loading and the sequence of the digital recorder voltage channels in relation to the load programming are shown in Figures 3 and 4. Table XI is a display of voltage recordings on each channel at six-hour intervals. Channels 20, 21, 34, and 35 represent voltages when all cathodes are under light load; numbers 24, 25, and 31 print when all are under heavy load. A comparison of 24 with 25, and 34 with 35 shows the effect of cathode location under heavy and light loads, respectively. The recordings on 21 and 31 were used to compute the cell output as shown in Table I of the Appendix. The anode current density was based on the combined areas of one face of each anode.

Cell P-73 was anode limited. Cell P-80 was approximately balanced with respect to anodes and cathodes. Cell P-93 featured extra anodes. At 42 hours the differences between channels 31 and 33 were 0.37, 0.18, and 0.07 volts respectively showing that high anode current density is most detrimental but that the cathode may be even three layers thick without excessive voltage loss. Note the current for the last cathode must pass through the electrolyte pores of the first and the second!



FORM FM-100

Figure 3



FORM FM-100

Figure 4

TABLE XI

## PERIODIC CELL VOLTAGES

### Cell No. P-80 Refer to Figure 3

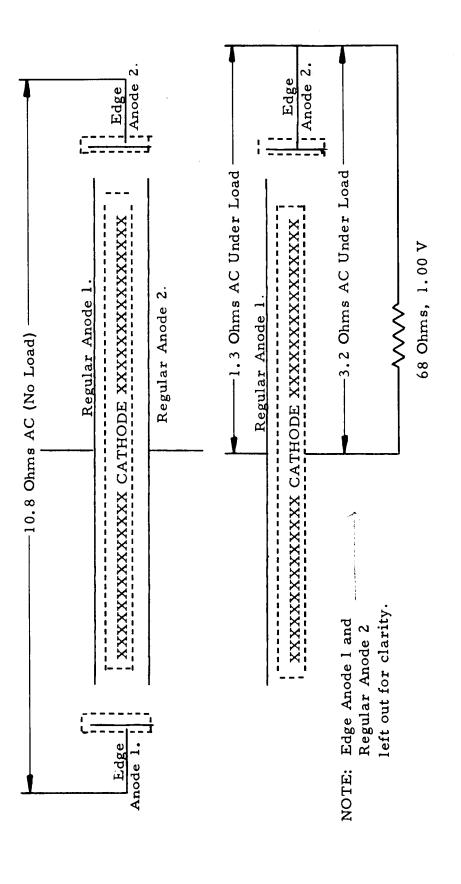
Elapsed Time	Channel Numbers										
(Hours)	20	21	22	23	24_	25	31 32	2	33	34	35
First		1.92	1.84	1.68	1.72	1.65	1.76 1.	72	1.74	1.91	1.87
6		1.95	1.90	1.80	1.77	1.66	1.75 1.	74	1.75	1.93	1.90
12		1.95	1.89	1.81	1.76	1.65	1.70 1.	71	1.72	1.92	1.89
18		1.93	1.90	1.79	1.75	1.62	1.63 1.	65	1.69	1.91	1.88
24	1.92	1.94	1.90	1.78	1.72	1.62	1.62 1.	63	1.67	1.90	1.88
30	1.91	1.94	1.89	1.76	1.69	1.58	1.56 1.	59	1.64	1.88	1.87
36	1.89	1.90	1.83	1.70	1.58	1.48	1.49 1.	54	1.61	1.86	1.85
42	1.86	1.86	1.75	1.59	1.45	1.37	1.34 1.	41	1.52	1.81	1.80
48	1.84	1.83	1.70	1.54	1.37	1.30	1.28 1.	38	1.50	1.80	1.79

## Cell No. P-93 Refer to Figure 4

	20	21_	22	23	24_	25	31	32	33	34_	35
First		1.93	1.86	1.75	1.71	1.61	1.76	1.73	1.69	1.92	1.89
6		1.95	1.89	1.78	1.67	1.57	1.77	1.73	1.71	1.93	1.89
12		1.96	1.91	1.79	1.69	1.49	1.72	1.73	1.71	1.92	1.90
18		1.94	1.88	1.73	1.67	1.50	1.66	1.69	1.68	1.91	1.88
24		1.91	1.84	1.70	1.65	1.50	1.62	1.66	1.65	1.90	1.84
30		1.91	1.84	1.68	1.63	1.48	1.60	1.64	1.62	1.90	1.85
36		1.90	1.81	1.65	1.60	1.45	1.55	1.59	1.58	1.88	1.81
42		1.86	1.73	1.57	1.50	1.37	1.46	1.50	1.53	1.83	1.78
48		1.82	1.67	1.50	1.41	1.28	1.37	1.41	1.47	1.80	1.74
54						1.22					
60		1.75	1.55	1.30	1.25	1.15	1.21	1.28	1.38	1.72	1.68

#### 2.6.2. Edge Discharge, Cell No. P-55

This was a conventional HgSO<sub>4</sub>/S/C prismatic cell with a single cathode and an anode on either side. In addition, narrow anodes were located to face two opposite edges of the cathode. Figure 5 is a cross-sectional schematic of this exploratory cell. The edge anodes were initially used as the working anodes against the cathode located perpendicularly and lengthwise to the edge anodes. Despite the long and narrow electrolyte path between the edge anodes and the working cathode, the early cell cut-off was attributed to anode polarization rather than electrolyte IR drop as indicated by Table XII. Subsequent to the initial discharge, the normal anodes were utilized as working anodes, the edge anodes used as references, and cell performance resumed for a substantial period of time. Since the reference electrodes were not in a favorable position to differentiate between anode polarization and electrolyte IR drop, it was not certain that anode polarization was responsible. The reference electrode should be placed in a favorable position between the working anode and cathode in order to discriminate between anode and cathode polarization. The reference in that case has to be perforated (Exmet). A complex cell, including this feature and several others, is presented under the next subsection.



CROSS-SECTIONAL SCHEMATIC OF CELL P-55

Figure 5

#### TABLE XII

#### REFERENCE READINGS, CELL NO. P-55

After 23 hours discharge via edge anodes, large anodes (reference) and small anodes (working) at 68 ohm load:

Cathode to Small Anodes	1.00V
Cathode to Large Anodes	2.10V
Large Anodes (+) to Small Anodes (-)	1.10V

Same readings with cell on open circuit for 10 minutes:

Cathode to Small Anodes	2.23V
Cathode to Large Anodes	2.10V
Large Anodes (-) to Small Anodes (+)	0.12V

Calculations (Refer to Figure 5):

$$I = \frac{E}{R}$$
 where

I = Cell current

E = Working cell voltage

R = External load resistance

I = 1.00/68 = 0.0147 amperes.

Ir where I = Cell current above

r = Cell ohmic resistance determined by ac measurements

Internal Ir loss =  $0.0147 \times 3.2 = 0.047 \text{ volts}$ .

Consequently, the potential of the cell has been reduced by ohmic polarization at the small anodes, not by Ir drop in the cathode.

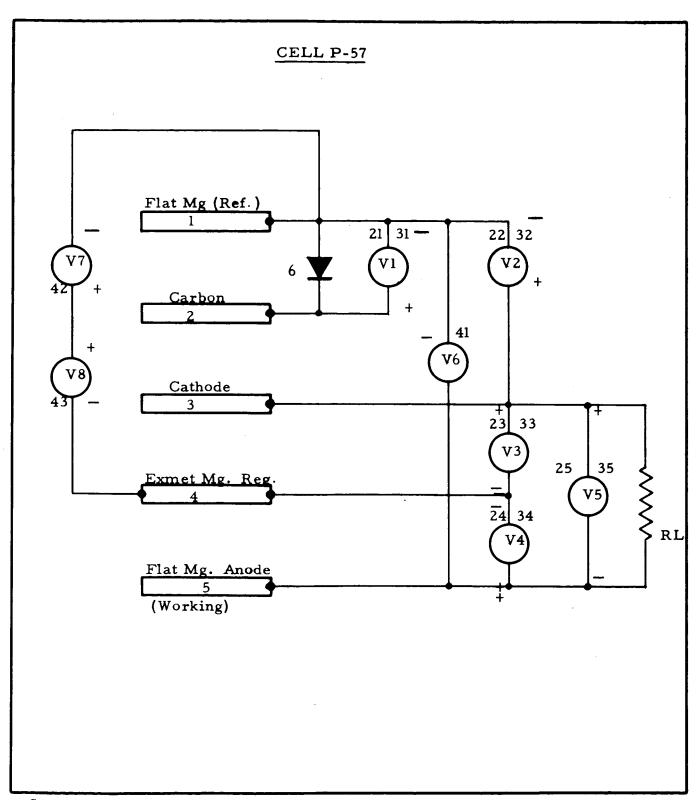
#### 2.6.3. Exploratory Flat-Plat Cell No. P-57

This cell (Figure 6) incorporated two flat magnesium anodes (I and 5) and a design center cathode (3)1. However, in between one anode (1) and the cathode (3) a pasted carbon electrode (2) was inserted, and between the other anode (5) and the cathode (3) an expanded magnesium anode (4) was located. actual load was applied between the cathode (3) and the working anode (5). was the anode (5) which was separated from the cathode (3) by means of the expanded magnesium reference electrode (4). As mentioned under paragraph 2.6.2., this reference electrode (4) which was between the cathode (3) and the single working anode (5), indicated clearly that voltage decline was due to loss of potential at the anode under load (5). The carbon electrode (2) was loaded by means of a diode (6) in the forward mode in order to determine the presence of soluble oxidants emanating from the cathode (3). While considerable current could be drawn from this carbon electrode (2) in the 1-volt region, little capacity was available in the 1.5 volt region. Considerable data was collected on this cell, but the significant points have been described, and these points will be further discussed in specific cells designed to illuminate these particular properties.

#### 2.6.4. Pasted Carbon Third Electrode Between Working Electrodes

The purpose of the following was to determine if sulfur or other oxidizing value was going into solution in the electrolyte and becoming lost to the cathode. In cell P-69, a porous carbon electrode was located between the single working anode and the single working cathode. The heavy 6-minute load was connected between the cathode containing sulfur only as the oxidant and the anode. The carbon electrode was connected to the anode via the light load which was left in place continuously. The carbon electrode did not show evidence of soluble oxidizing value until late in the run. This was certainly an informative and unexpected turn of events since the higher polysulfides are soluble in liquid ammonia.

<sup>&</sup>lt;sup>1</sup> (R efer to Figure I, Appendix B, page B-2. A "design center cathode" consists of 20 grams of HgSO<sub>4</sub>, 4 grams of sulfur and 12 grams of graphite and has the capability of providing 1/5 of the capacity required of a full-sized cell at -90°C. Examples of cells with this cathode are P-14, 51, and 52.



FORM FM-100

Figure 6

## 2.6.5. Single Cathode, Two Anodes Loaded Individually-Cell No. P-134

Since each anode was loaded with one half of the normal total, the overall current density was the same as that of a conventional prismatic cell. The heavy and light loads were applied sequentially to each anode, and the performance of each was monitored continuously. Figure 7 is a schematic drawing of the electrodes and the electrical loading and shows the sequence of the digital voltage recordings. Table XIII is a display of the voltages on each channel at twelve hour intervals. The normal duration of the heavy load is six minutes (10 channels x 36 seconds per channel). In this case, only 50 percent of the heavy load was applied to the cathode during the print-out of channels 3, 4, 13, and 14; and 100 percent during the print-out of channels 5 through 12. Thus, four channels at 50 percent of full load plus eight channels at full load are equivalent in terms of watt-minutes to 10 channels at 100 percent heavy load.

In general, the performance of the two anodes was much the same. As expected, the potential dropped as the load was increased and then recovered as the load was decreased. The effect of increased current density on the cathode is shown by channels 3 vs 5.

Further data reported on this cell is presented in 2.6.6.1.

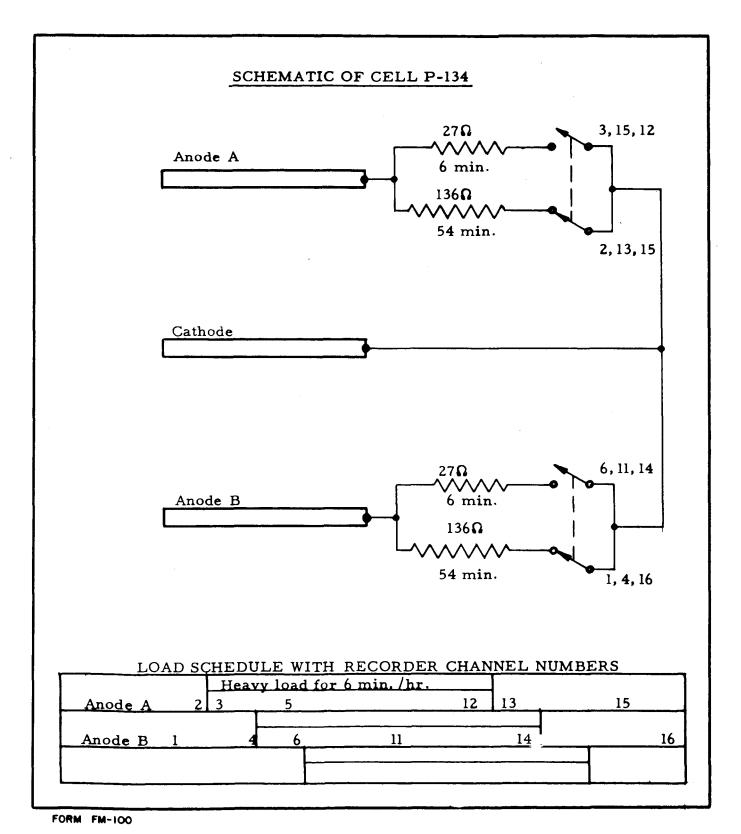


Figure 7

TABLE XIII

# PERIODIC CELL VOLTAGES

# Cell No. P-134

# Refer to Figure

Anode:	В	Α	A _	В	Α	В	В	Α	Α	В	A	В
Channel No.	1	2	3_	4	5	6_	11	12	13	14	15	16
Hours	ı		1		l				ı		ı	
1	1.87	1.87	1.75	1.82	1.70	1.68	1.72	1.73	1.83	1.78	1.88	1.90
12	1.91	1.91	1.80	1.87	1.77	1.76	1.72	1.68	1.83	1.67	1.87	1.86
24	1.91	1.90	1.79	1.87	1.74	1.74	1.70	1.61	1.83	1.65	1.86	1.86
36	1.89	1.89	1.77	1.84	1.69	1.70	1.58	1.58	1.79	1.60	1.84	1.85
48	1.82		ı				1.48		1		1.78	
60	1 90	1.90	1 77	1 86	1 71	1 70	1 62	1.65	1 82	1.59	1 86	1.86
72	1.84		1.61		1.51		1.43		1		ł	1.82
	1 02		1								1.77	1 79
84 96	1.82		4				1.42		1	1.45 1.36	l .	1.73
	<del></del>				<u> </u>						1	<del> </del>
108	ł:	1.73			L				1		1	
114	1.65	1.64	1.39	1.52	1.27	1.25	1.20	1.19	1 . 44	1.26	1.55	1.58
	Lt.	load	_		He	avy lo	ad			3>-	Lt.	load
	54 m	in/hr.			6 n	nin./h	$\mathbf{r}$ .				54 m	nin./hr
	Ţ		<b>4</b> −50	% <b>→</b>		100%	<sub>0</sub>	>-	<b>▼</b> 5	0% >		
	1			,-		<b>,</b>	-	-				
	1								1			
	í		!		1				1		1	

#### 2.6.6. Cell Resistance and Capacitance

A Kelvin ac bridge with a phase-sensitive null indicator was constructed and used to measure the subject characteristics of cells during discharge.<sup>2</sup> A diagram of the circuitry is shown in Figure 8. In order to avoid interruption of continuous cell discharge, the bridge was connected in parallel with the cell circuit. The computation of the resistance of Cell No. B-59 from the bridge measurements is presented as an example.

Heavy load resistor,  $R_1 = 2.7\Omega$ 

Standard resistor,  $R_s = 1.35\Omega$ 

Standard capacitor  $C_s = 24950$  microfarads, with  $0.0695\Omega$  equivalent series resistance as measured by the bridge in calibration procedures.

 $R_{+} = 0.311\Omega$  (total calculated from bridge readings)

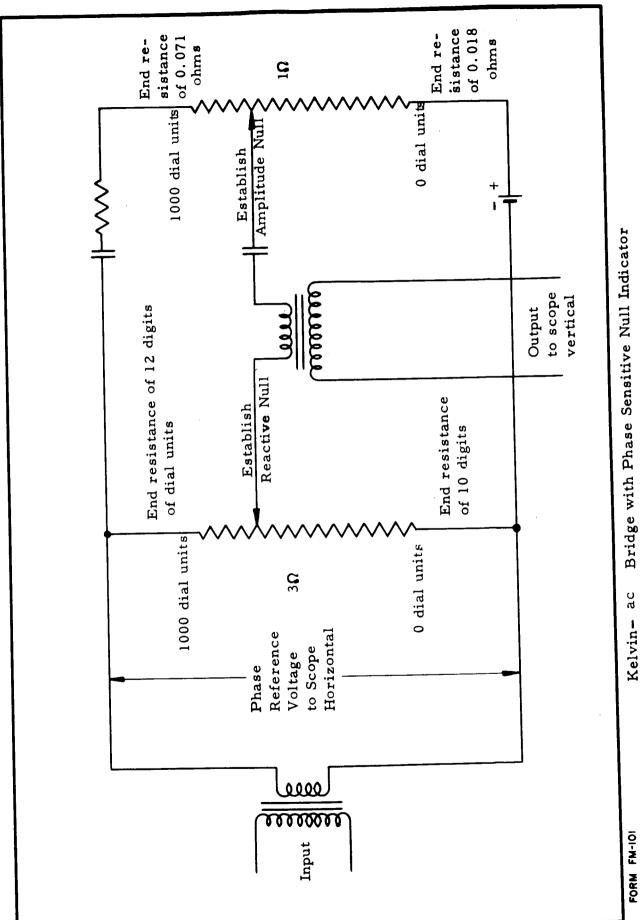
R<sub>u</sub> = unknown cell resistance, calculated from the formula for parallel resistances, as follows:

$$1/R_{t} = 1/R_{u} + 1/R_{I}$$
;  $1/0.311 = 1/R_{u} + 1/2.7$ ;  $R_{u} = 0.351\Omega$ 

For the purpose of these studies, the difference of  $0.04\Omega$  is negligible for comparative purposes. In the case of the 13.5 $\Omega$  light load resistor, the correction is insignificant.

The resistance and capacitance values under light and heavy loads are plotted against the current and extrapolated to zero current.

<sup>&</sup>lt;sup>2</sup>"Storage Batteries, "Vinal, 4th Edition, Pages 318 - 331, John Wiley & Sons, Inc., New York, 1955.



Kelvin- ac

Figure 8

## 2.6.6.1. Resistance and Capacitance of Prismatic Cell

Cell No. P-134, which had one cathode and two separately loaded anodes, is described in Section 2.6.5. and illustrated in Figure 7. The data in Table XIV seem to indicate that the origin of the capacitance values in the system,  $Mg/KSCN:NH_3/S$ , is in the anode.

TABLE XIV

Resistance and Capacitance of Prismatic Cell No. P-134

	Elapsed	Anode A to		Anod	le B to	Anode to		
	Time	cat	hode	ca	thode	6	anode	
	hours	mF	ohms	mF	ohms	mF	<u>ohm s</u>	
Light load	4	16.8	0.68	17.8	0.40	9.2	0.98	
Heavy load	4	13.4	0.74	15.4	0.76	7.7	1.12	
X*	4	(a) 17.9	0.66	(a)19.5	0.36	(a)10.4	0.92	
Light load	24	17.8	0.78	19.0	1.35	9.9	1.38	
Heavy load	24	20.0	0.75	19.0	0.81	9.9	1.26	
X*	24	17.0	0.79	19.0	1.54	9.9	1.70	
Light load	47	13.9	0.82	13.8	1.58	7.3	1.39	
Heavy load X*	47 47	13.1 14.0	0.99 0.78	13.8 13.8	0.85 1.78	6.3 7.4	1.43 1.38	

<sup>\*</sup>X = values obtained by extrapolation to zero current.

#### Verification:

$$1/C_a + 1/C_c = 1/C$$

Where C = Anode A to cathode, capacitance value

C<sup>a</sup> = Anode B to cathode, capacitance value

C<sup>c</sup> = Anode A to anode B, capacitance value

$$1/16.5 + 1/19.5 = 1/9.0$$

Therefore, cathode capacitive reactance is negligible, particularly during the first day of discharge.

Capacitance in millifarads (mF)

The 60 cycle ac impedance of the cells results largely from the anode to electrolyte capacitance, cell resistance, and cathode capacitance in series. The measured value of cell capacitance appears to be limited by the anode active area since the cathode capacitance is quite high.

#### 2.6.6.2. Effects of Mercuric Sulfate in Bobbin Cells

The addition of of small amounts of HgSO<sub>4</sub> to the cell system of the preceeding paragraph appears to increase the effective anode area substantially, and the capacitance values observed after the required life had been exceeded may indicate cathode polarization. The data are presented in Table XV.

TABLE XV

Resistance and Capacitance of Bobbin Cells Containing HgSO<sub>4</sub>

Cell	Elapsed Time	Cell life	Cell	Ligh	t load	Heavy	load	3	X*
No.	hours	to 1.3V	Size	mF	ohms	mF	ohm s	mF	ohms
B-57	16 92	84	1/2	32 5	0.17 1.46	28 7.5	0.18 1.14	25 12	0.20 1.64
B-58	16 93	106	1/2	45 19	0.55	50 21	0.52 0.51	55 23	0.50 0.55
B-59	17 40 64 138	111	full	41 82 39 28	0.38 0.23 0.33 0.85	40 50 41 22	0.31 0.24 0.33 0.81	42 47 46 20	0.33 0.25 0.33 0.80

<sup>\*</sup>X = values obtained by extrapolation to zero current Capacitance in millifarads (mF).

#### Cathode Composition:

	B-57	B-58	B-59
	_%	<u></u> %	%
HgSO <sub>4</sub>	**	9.5	9.5
Sulfur	50	45	45.2
Graphite	40	36	36.3
Acetylene Black	10	9.5	9.0

<sup>\*\*</sup>Electrolyte saturated with HgSO<sub>4</sub> (about 0.1%)

#### 2.6.6.3 Resistance and Capacitance of Bobbin Cells

A summary of the measurements taken on 15 cells is shown in Table XVI. While the object of this tudy was to build a background of valid resistance readings in the face of series capacitive reactance, it was found that capacitance was more significant than resistance (as long as R was reasonable). Capacitance values decrease markedly near end of cell life. While the cells of Table XVI include many construction and test variations, the general trend of decreasing capacitance with continued discharge is quite evident.

The last column of Table XVI summarizes the resistance data and shows that the internal cell resistances are generally of the order of 10 percent of the value of the heavy load resistor prior to cut-off.

TABLE XVI

Resistance and Capacitance of Bobbin Cells

# Cells Identified in Table II of Appendix A

				Elapsed		
Cell No.	Cell life	Temp.	Cell	Time		
B	to 1.3V	<u>°C</u>	Size	hours	mF*	ohms*
50	61	-90	full	23	125	0.15
				46	52	0.30
51	69	-90	full	23	87	0.25
		i		45	57	0.35
52	68	-90	full	24	25	0.27
				<b>4</b> 5	24	0.57
53	59	- 90	full	22	98	0.25
				45	38	0.37
54	113	-90	1/2	18	57	0.55
			i	<b>4</b> 1	28	0.67
				118	47	0.63
55	72	<b>-</b> 90	full	72	45	0.62
56	76	-63	1/2	69	247	0.37
				89	168	0.45
57	84	-90	1/2	16	25	0.20
	<u> </u>			92	12	1.64_
58	106	-90	1/2	16	55	0.50
	<u> </u>			93	23	0.55
59	111	-90	full	17	42	0.33
	[			40	47	0.25
	]			64	46	0.33
				138	20	0.80
60	127	-40	1/2	12	78	0.28
				40	43	0.25
	1			64	60	0.35
				138	7	0.35
61	176	-63	1/2	16	160	0.33
				186	7	1.60
62	82	-90	1/2	16	147	0.35
	1		ļ	40	60	0.47
	<u> </u>			114_	5	1.83
63	101	-73	full	16	≈lF	0.37
	1			89	252	0.35
		· · · · · · · · · · · · · · · · · · ·		111	125	0.47
64	97	-73	full	16	475	0.26
	<b>{</b>			40	475	0.14
	l [			112	90	0.10

<sup>\*</sup> Values obtained by extrapolation to zero current.

Capacitance in millifarads (mF): Resistance in ohms.

#### BOBBIN CELL DESIGN, CONSTRUCTION AND TESTING

Since cylindrical cells offer many advantages over prismatic cells in simplicity and ease of construction, the development of bobbin cells was started in the second quarter. The knowledge gained in contract NAS 3-6009 and from the prismatic cell studies was used as a basis where applicable. A general description of the method of construction, cross-sectional sketches and drawings may be found in Appendix B.

## 3.1. Preliminary Designs for Task I

Nos. B-1, 2, and 3 were of simple construction with central rod anode and annular ring cathode. Since all three seemed short of life because of insufficient anode area, the rod anodes were replaced by cylindrical coils made of AZ31B Mg Exmet. This modification was beneficial and yielded longer cell life. The improvement was approximately proportional to the increase in apparent anode area in cells B-4 through B-7. This relationship was held for B-7 even though much of the additional area was provided by the use of external anodes in conjunction with the central coil. It is surprising that the proportionality between Nos. B-6 and 7 remained a direct ratio since the change in geometry permitted discharge in two directions from the cathode rather than the single-sided discharge of all of the preceding bobbin cells.

Following these cells, five designs (Nos. B-8 to B-12) were constructed and placed on discharge at -90°C. Unfortunately, the refrigerator malfunctioned badly and permitted the temperature to rise as high as -66°C, with an average of about -81°C. Consequently, the test results are of little value, except that they indicate that center bobbins (B-10 and 11) seem to function poorly. Cell No. B-8, which had a center coil of Mg Exmet surrounded by an annular ring cathode and a double Exmet anode on the outside of the cathode, provided the longest life.

Because of the poor temperature regulation, it was necessary to build similar cells, B-13 through 16. The central bobbin cathode with outside anodes (B-14) gave the poorest results; a central star-shaped anode with ten longitudinal fins and the cathode mix between the separator and the case (B-15) provided the longest life, 62 hours to 1.3 volts. In this type of cell, the cathode was in the form of a thin-walled cylinder, and the conductive case served as the collector. Since the B-15 configuration seemed to be the best, it was adopted for all subsequent tests in this phase of the program. Any modifications to this basic design will be explained in the later sections.

#### 3.2. Electrolyte Studies at -90°C

During the discharge of the Mg/KSCN/S type cells the K<sup>†</sup> ion is converted to an equivalent of Mg<sup>++</sup> ion. The spent electrolyte  $\left[\left(\frac{1}{2}\text{Mg}(SCN)_{2}\right)\right]$  should by theory, be superior to the initial electrolyte since the couple Mg/Mg<sup>++</sup> is now defined. Spent electrolyte was used alone and in combination with virgin KSCN/NH<sub>3</sub> solutions. Some cells were activated with 34% KSCN; others, with 25% KSCN. The composition of the cathode was varied also. The test results are summarized in Table XVII.

TABLE XVII

Electrolyte Studies

			Electrolyte(Wt. % as KSCN)								
Cell No.	S	С	Acet. Blk.			50% Virgin	Hour	s to≉			
B-	<u></u> %	<u></u> %	<u></u> %	Virgin	Spent	50% Spent	1.5V	<u>1.3V</u>			
15	70	30	0	34			54	62			
17	70	30	0		25		36	63			
19	50	45	5		25		80	91			
23	50	45	5	34			66	73			
24	50	45	5			25	71	84			
26**	50	45	5	34			56	67			
27**	50	45	5	25			40	47			
30	50	40	10	34			68	76			
31	50	40	10	25			43	53			

<sup>\*</sup> Under heavy load.

The change to spent electrolyte in B-17 was not beneficial. In B-19, the following changes were made:

- a. Spent electrolyte was used.
- b. The proportion of graphite to sulfur was increased.
- c. 5% acetylene black was added.
- d. The total cathode weight was decreased from 120 to 89 grams.

The combination proved to be good by increasing the cell life to 91 hours to the

<sup>\*\*</sup> Ball-milled.

1. 3 volt cut-off. The fact that B-23 with virgin electrolyte ran only 73 hours indicates that the spent electrolyte was responsible for part of the gain. The voltage under heavy load of B-23 ran from 0.2 to 0.1 volt above that of B-19 during the first 55 hours, after which it decreased rapidly to the 1.3 volt cut-off at 73 hours. The use of half-spent electrolyte in B-24 again demonstrated its contribution by extending the cell life from 73 hours to 84 hours.

The more concentrated electrolyte (34% vs 25%) was shown to be much superior, as may be seen by a comparison of B-26 with 27 and 30 with 31. It seems probable that a cell such as B-19 could be improved through the use of a 34% spent electrolyte.

Attempts were made to synthesize Mg(SCN)<sub>2</sub> by the reaction of magnesium with a solution of NH<sub>4</sub>SCN in liquid ammonia but there is some doubt about the composition of the reaction products. This electrolyte was used in cells B-20 and 21, and a mixture of 1 part of this to 9 parts of virgin KSCN solution was used in B-29. None of these cells discharged well. Other methods of preparing Mg(SCN)<sub>2</sub> are being considered.

## 3.3. Ball-Milling of Cathode Mix

The cathode ingredients were mixed as a slurry in heptane in a ball mill in order to obtain a more intimate mixture and, consequently, improved cell performance. After milling for 24 hours, the slurry was removed from the jar, and the heptane was removed by evaporation. The resultant soft cake was pulverized manually and packed into the cathode space of the cell B-26 in the usual manner.

A comparison of the life of this cell with No. B-23 (Table XVII) shows a reduction from 73 hours to 67 hours under the same discharge conditions. Although nothing was gained by this extra milling procedure over the usual manual method, some advantage might be gained by a study of the effects of other mechanical devices.

# 3.4. Variations in Proportions of Graphite (C), Acetylene Black and Sulfur

In the following table, the effects of changes in cathode composition are shown. All cells were activated with 34 weight percent KSCN in ammonia and were discharged at -90°C.

TABLE XVIII

Cathode Composition Variations

## Half-sized Cells:

Cell No.	S %	C %	Acet. Blk.	Cath. Wt. Total gms.	Cathode Density g/in. <sup>3</sup>	Hour 1.5V	s to* 1.3V	F/mol Sulfur
15	70	30	0	120	11.8	54	62	0.08
25	50	50	0	89	8.7	51	51	0.12**
23	50	45	5	89	8.7	66	73	0.17
30	50	40	10	96	9.4	68	76	0.17
32	50	0	50	70	6.9	67	75	0.22
Full-size	ed Ce	lls:						
50	50	40	10	192	9.4	56	61	0.13
51	50	40	10	192	9.4	62	69	0.15
52	40	50	10	192	9.4	61	68	0.18
28	50	30	20	192	7.9	53	57	0.14
52	40	40	20	192	7.9	59	59	0.19

<sup>\*</sup>Under heavy load.

It is apparent that acetylene black improved the efficiency of sulfur utilization and the cell life of the half-sized cells. About the same number of hours were obtained with 5, 10 and 50 percent acetylene black, and all of these cells performed better than the cathodes containing 50 percent acetylene black, yielded the highest efficiency and a 75-hour life to 1.3 volts. However on that cell, the powders were very difficult to mix and pack in the dry state; so they were mixed in heptane, the slurry was poured into the case and then the anode in its separator cup was forced down into position through the slurry. Finally, the cell was dried in a vacuum chamber for two days before activation. The cathode

<sup>\*\*</sup>Between the 51st and 53rd hours, the discharge curve dropped 0.45 volts under heavy load-reason unknown.

of B-30, with 10 percent acetylene black, seemed to be about the best based on handling qualities of the mix and coulombic output of the cell. The optimum composition and degree of compaction cannot be determined with such a limited number of experiments.

# 3.5. Task I.B., Construction of the Five (5) Ammonia Cells Most Likely to Operate at -90°C for 72 Hours

The specifications for the construction and testing of the subject cells were submitted to and approved by the Project Manager. These are given in Table XIX and Figures 9 and 10.

#### TABLE XIX

	Task I. B., Construction/Load Specifications							
CATHODE:	Sulfur (grams/%)	96/50						
	Carbon (grams/%)	77/40						
	Acetylene black (grams/%)	19/10						
	Total cathode wt., grams	192						
	Thickness of annular ring (in.)	0.30						
	Length (in.)	13.5						
	Collector	CAB-XL Case						
ANODE:	AZ31B Mg Sheet	10 longitudinal fins						
	Apparent Area (cm²)	354						
ELECTROLY	TE (liquid NH <sub>3</sub> solvent):							
	KSCN (weight %)	34						
	Volume (cc)	575						
NET CELL V	OLUME (in. 3)	43						
LOAD ( $\Omega$ ):		2.7 for 6 mins.						
		13.5 for 54 mins.						

The first set of five (5) cells (Nos. B-33 to 37) tested under this requirement provided an average life of 61 hours, with a maximum of 70 hours and a minimum of 53 hours under heavy load to the 1.3 volt cut-off. The cathodes were packed by tamping with a rod, an unsatisfactory method for a full-sized cell. As a result, only 170 grams were used, rather than the 192 grams desired.

To simplify and improve the packing, an annular sleeve piston was fabricated to press the cathode mix into place. In building B-42, 24 ten gram (240g total) increments of the mixture were added. To each addition, the maximum manual pressure was applied, and it was found that the depth of each increment was very constant at 9/16 inch, for a total of 13.5 inches. A run time of only 61 hours indicated that this cathode was too dense. The large quantity of oxidant yielded only 0.10 faraday per mol.

Therefore, in the second set of five (5) cells (B-43 to 47), 192 grams of the cathode mix were used. Each of ten 19.2 gram portions was added and pressed with the piston to 1/10th of the total depth of 13.5 inches. When discharged, an average life of 64 hours was achieved, with a maximum of 77 hours and a minimum of 58 hours.

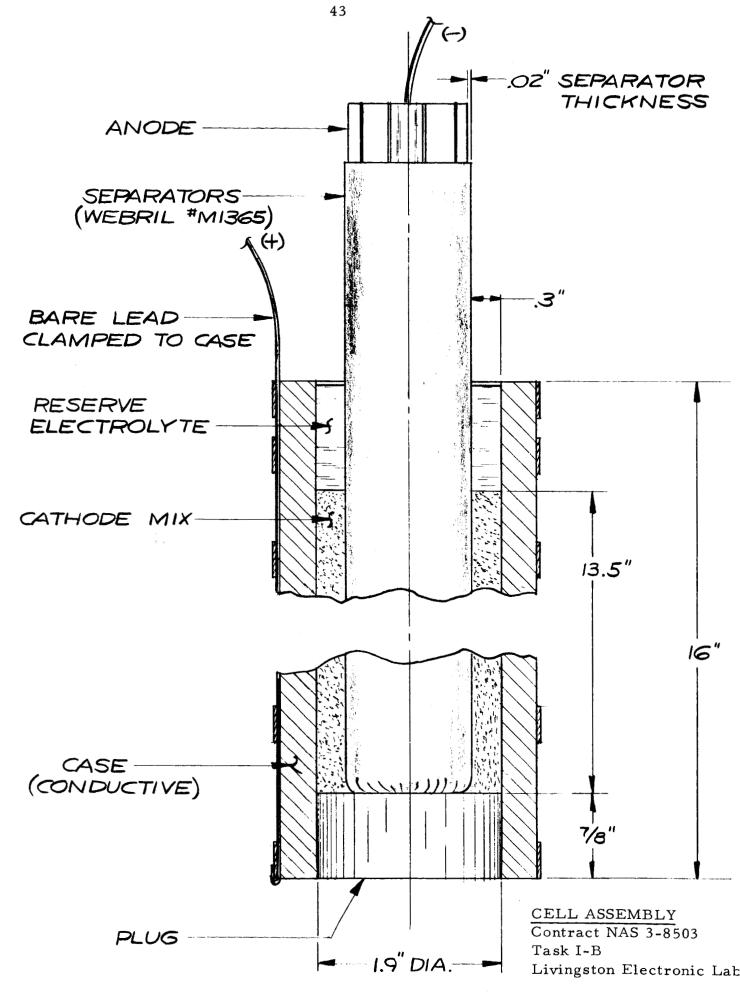
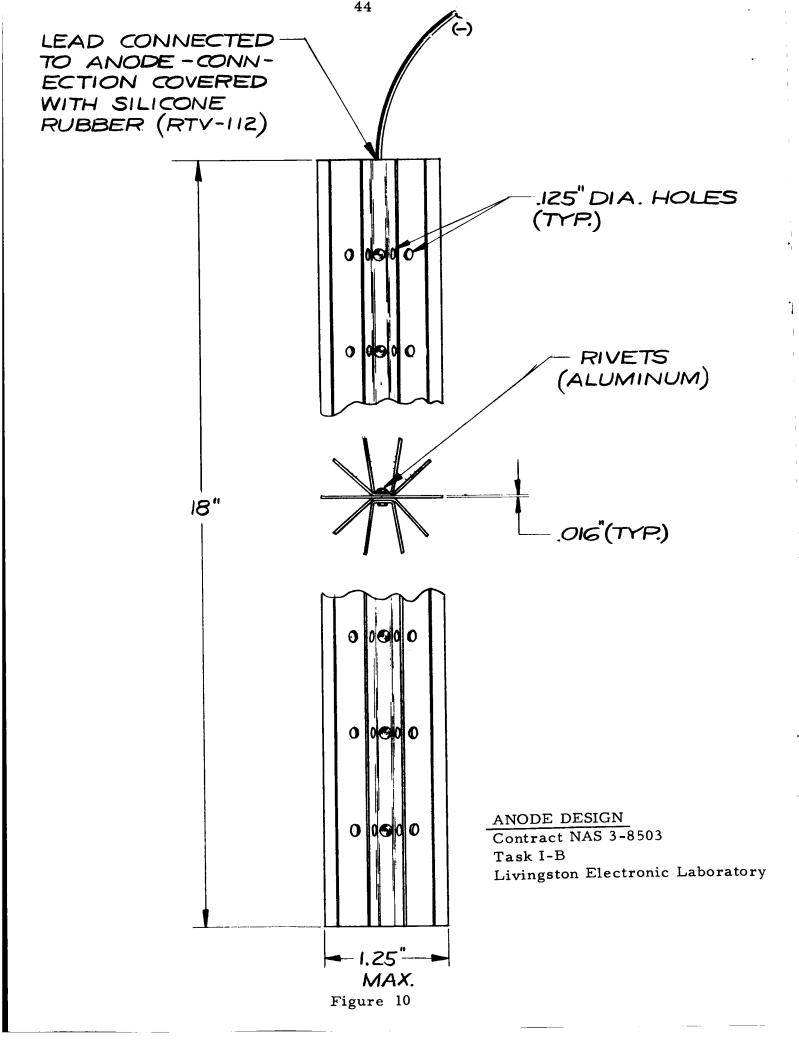


Figure 9



#### 3.5.1. External Resistance

Resistance measurements indicated the need to employ double lead wires between the cells and the loads and more collector clamps on the cases. These modifications were adopted in subsequent cells as shown in Table II of the Appendix. A comparison of cells B-50 and 51 with B-43 to 47 shows a modest improvement, particularly in the maximum voltage under heavy load. The average increased from 1.72 to 1.79 volts.

#### 3.6. Mercuric Sulfate/Sulfur Cells

In an attempt to extend the cell life beyond that achieved in Nos. B-43 to B-47 and to exceed, if possible, the goal of 72 hour operation, experiments were conducted with HgSO<sub>4</sub> as an additive to the S/C cathode. A number of such cells were tested in the current configuration which uses an outer annular cathode and a finned anode in the center. The results are given in Table XX along with those of two cells T-60 and T-119 built under Contract NAS 3-6009. The latter cells had center bobbin cathodes surrounded by cylindrical sheet anodes.

TABLE XX

Mercuric Sulfate/Sulfur Cells

Cell	$HgSO_4$	S	Graphite	Acet. blk.	Cath. wt.	Wt. %	Temp.		s to*
No.	g	g	g	g	g	KSCN	<u> </u>	<u>1.5V</u>	<u>1.3V</u>
B-56	53	10	45	5	113	25	-63	68	76°
T-60	106	20	60	0	186	25	-63	106	119
			- 0		221	2.4	0.0	50	7.0
B-55	106	20	90	10	226	34	-90	59	72
T-119	106	20	60	0	186	34	-90	21	27
D 54	10	4.0	20	10	106	34	-90	101	113 <sup>c</sup>
B-54	10	<b>4</b> 8	38	10			-		113 C
B-58	10	48	38	10	106	34	-90	96	106°
B-59	20	96	77	19	212	34	-90	95	111
D [5		4.0	20	10	06	2.4	0.0	64	84 <sup>c</sup>
B-57	a	48	38	10	96	34	-90		
B-62	b	48	38.5	9.5	96	34	-90	71	82 <sup>c</sup>
B-61	10	48	38.5	9.5	106	34	-63	158	176°
				·					127°
B-60	10	48	38.5	9.5	106	34	-40	97	121

<sup>\*</sup>Under heavy load.

Cell No. B-56, containing the same ratio of HgSO<sub>4</sub> to S as T-60, was tested at -63°C to compare the performance in the two configurations. Additional graphite and acetylene black were added to extend the cathode length and thereby utilize

<sup>&</sup>lt;sup>a</sup>The electrolyte was saturated with HgSO<sub>4</sub> (about 0.1%)

bSeven (7) grams of HgSO<sub>4</sub> were wrapped and sealed in a cylindrical capsule of Webril separator paper and placed in the anode compartment.

<sup>&</sup>lt;sup>c</sup>Half-sized cells: the resistive loads were adjusted accordingly.

comparable anode areas. B-56 was definitely inferior to T-60 and did not meet the 72 hour requirement to the 1.5 volt cut-off. On the contrary, the use of the current configuration in B-55 at -90°C yielded results that were far superior to those obtained from cell No. T-119.

9.5 percent HgSO<sub>4</sub> was added to the S/C cathode of cell No. B-54. The performance of this cell represents an outstanding improvement in life at -90°C; 101 hours to 1.5 volts and 113 hours to 1.3 volts. Excellent replication was achieved with B-58, another half-size cell, and with B-59, a similar full-sized cell. Nos. B-57 and 62 which had HgSO<sub>4</sub> in the anode compartment did not run as long as those having it in the cathode, but they were much better than the two preceeding groups of five (B-33 to 37 and 43 to 47) which did not contain any HgSO<sub>4</sub>.

Nos. B-61 and 60 were discharged at -63°C and at -40°C, respectively, to determine the performance characteristics of the  $HgSO_4/S$  cathode at higher temperatures. The results were beyond all expectations; 158 hours at -63° and 97 hours at -40° to an end voltage of 1.5. Sulfur/carbon cathodes, without  $HgSO_4$ , ran at -63° for 53 hours to 1.5 volts (B-38 and 39) and at -40° for 91 hours to the same end voltage (B-40 and 41).

## 3.7. Task II, Design

A self-contained ammonia cell, excluding activator, was designed for the purpose of fabricating a number of such cells for test or delivery to NASA. The advantages and disadvantages of the various features, as depicted in numerous preliminary sketches, were discussed with LEC personnel and the Project Manager. The cell which met with the approval of all concerned is illustrated by drawings B-1227, B-1228, A-1238, and A-1239 and is further defined by the Parts and Materials List; all of which may be found in Appendix B, together with a general description of the method of construction. It was designed to accommodate electrodes of the type used in cell B-59 and to perform in accordance with the contract specifications.

## 3.8. Task III, Test and Redesign

Two mockup cells, B-63 and 64, were constructed, based on the approved design from Task II. Since the assembly procedures were satisfactory, it was decided to evaluate the units by activation and discharge at -73°C. The results were most gratifying: Cell B-63 ran 81 hours to 1.5V, 101 hours at 1.3V; Cell B-64 ran 87 hours to 1.5V, 97 hours to 1.3V. Additional data on these cells may be found in Table II of Appendix A.

#### FUTURE WORK

Task III-A will be completed next month by building and testing five cells. The design will be based on the approved design drawings from Task II. In this first set of five cells, the anode must be fabricated from sheet and rod stock. As soon as the extruded anodes become available, the second group of five cells will be constructed and tested to satisfy the requirements of Task III-B. The delivery date of the anodes was estimated by the manufacturer to be October 19, 1966.

In addition, the cathode formulation will be improved if possible by testing a series of cells covering a broad range of HgSO<sub>4</sub> content.

In other cells, substitutes for the "star" or finned anode will be tested. One will be a simple 1/2 inch diameter rod; another will be a 1-1/4 inch diameter cylinder with numerous holes for electrolyte passage.

APPENDIX A

#### NOTES TO TABLES

- a. Loads shown as A/B represent cyclic loads of A  $\Omega$  for 6 minutes and B  $\Omega$  for 54 minutes.
- b. Cumulative hours based on heavy load. Hours shown as A/B represent A hours to 1.5 volts and B hours to 1.3 volts.
- c. Based on lighter load.
- d. Based on heavier load.
- e. Based on "apparent" anode area.
- f. Mg rod, 1/2" dia., finned and fluted.
- g. Mg rod, 1/2" dia., four 1/8" x 1/8" vertical flutes.

#### MATERIALS IDENTIFICATION

- j. HgSO<sub>4</sub>. A. R. Grade; Mallinckrodt Chemical Works, St. Louis, Mo.
- k. Sulfur. Sublimed, Merck & Co., Inc., Rahway, N.J.
- kk. Sulfur. N.F. Sublimed powder, Matheson, Coleman & Bell, Norwood, Ohio
  - 1. Carbon. Air spun graphite, Type 200-44; Jos. Dixon Crucible Co., Jersey City, N.J.
- m. Binder. Polystyrene dissolved in toluene; (1.0g/100 ml).
- n. KSCN; Reagent; B & A. Code 2144; Allied Chemical Co., New York, N.Y. LEC Lot No. 8.
- nn. KSCN; Reagent; B & A. Code 2144; Allied Chemical Co., New York, N.Y. LEC Lot No. 9.
  - o. KSCN; Reagent; Fisher P-317, Lot No. 743879, Fisher Scientific Co., Pittsburgh, Pa. LEC Lot No. 7.
  - p. Pure Mg sheet. Dow Chemical Co., Midland, Michigan.
  - q. AZ31B Mg sheet. Dow Chemical Co., Midland, Michigan.
  - r. Silver-plated copper Exmet. Exmet Corp., Bridgeport, Conn.

#### Manufacturer's Designation: 20 Cu 30-2/0

Original metal thickness, 20 mils

Metal symbol, Cu (copper)

Strand width, 30 mils

Mesh designation, 2/0

s. Copper Exmet. Exmet Corporation, Bridgeport, Conn.

#### Manufacturer's Designation: 20 Cu 30-2/0

Original metal thickness, 20 mils

Metal symbol, Cu (copper)

Strand width, 30 mils

Mesh designation, 2/0

#### NOTES TO TABLES

#### MATERIALS IDENTIFICATION

- t. SM-91 Polypropylene non-woven fabric; .005" thickness per layer. The Kendall Co., Walpole, Mass.
- u. M-1365 non-woven acetate & cotton; 0.004"/layer. The Kendall Co., Walpole, Mass.
- v. MPR-Microporous rubber; .030"/layer. American Hard Rubber Co., Butler, N.J.
- w. Copper Exmet, silver-plated after having been cut to size.

Manufacturer's Designation: 20 Cu 30-2/0

Original metal thickness, 20 mils Metal symbol, Cu (copper)

Strand width, 30 mils Mesh designation, 2/0

ww. Copper Exmet, gold-plated after having been cut to size.

Manufacturer's Designation: 20 Cu 30-2/0

Original metal thickness, 20 mils Metal symbol, Cu (copper)

Strand width, 30 mils Mesh designation, 2/0

x. Pure Silver Exmet.

Manufacturer's Designation: 5 Ag 8-1/0

Original metal thickness, 5 mils Metal symbol, Ag (silver)

Strand width, 8 mils Mesh designation, 1/0

xx. Lead Exmet.

Manufacturer's Designation: 25 Pb 25-1/0

Original metal thickness, 25 mils Metal symbol, Pb (lead)

Strand width, 25 mils Mesh designation, 1/0

y. AZ31B Mg Exmet.

Manufacturer's Designation: 16 Mg 30-2/0E

Original metal thickness, 16 mils Metal symbol, Mg (magnesium) Strand width, 30 mils Mesh designation, 2/0E

- yy. Aluminum collector, 0.020" thick, Lincaine perforations, Item 33, Reynolds Aluminum Company.
  - z. Porous polyethylene tube, Bel-Art Products, Pequannock, N.J. 100 micron pore size, 1.0" O.D. x 5/8" I.D.
- zz. Aluminum Exmet.

Manufacturer's Designation: 20 Al 40-1/0

Original metal thickness, 20 mils Metal symbol, Al (aluminum) Strand width, 40 mils Mesh designation, 1/0

#### TABLE I

# ELECTROCHEMICAL CELL TESTS

Discharge Temperature: -90°C

Pasted Plate Configuration

Polyethylene Bag Vehicles

Cathode Collector: Silver-plated Exmet

Cathode Binder<sup>m</sup>: 0.2g Polystyrene in 20 cc Toluene for Std. 36g Cathodes Electrolyte: 34 Wt. % KSCN<sup>n</sup> in liquid ammonia

Electrolyte: 34 Wt. % KSCI	Thi fiquid as			
Cell No. P-	46	47	51	54
Major Variables	Thin Cath	odes	Same as P-52 No MPR	Thick Cathode
Hours to End Voltage (1.5/1.3V)	37/49	31/48	61/70	20/30
Cathode: HgSO <sub>4</sub> <sup>j</sup> (g)	5	5	20	100
Cathode: Sulfur <sup>k</sup> (g)	1	l	4	20
Cathode: Carbon (g)	3	3	12	60
Cathode: Paper Pulp (g)				1.8
Separator Thickness (in.), M1365 <sup>u</sup>	0.020	0.020	0.020	0.020
Separator Thickness (in.), MPR				~ ~ ~
Anode Area (cm²) AZ31B Mg	210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>q</sup>
Anode Reference AZ31B Mg			= -	<b></b>
Cathode Collector Area (cm²)	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>
Volume Electrolyte (cc)	100	100	100 + 50	350
Net Cell Volume (in.3)	7.5	7.5	7 . 5	27
Load <sup>a</sup> (ohms)	48/240	48/240	13.5/68	2.7/13.5
Initial Closed Circuit Voltage c	2. 24	2. 23	2.24	2.14
Peak Closed Circuit Voltage C	2.24	2. 23	2. 25	2.21
End Voltage (heavy load)	1.30	1.30	1.30	1.30
End Voltage (light load)	1.65	1.62	1.61	2.04
Peak Current Density d (mA/cm <sup>2</sup> )	0.22	0.22	0.76	3.42
Obs. Coulombs/g Total Oxidants	304	298	393	165
Observed F/mol Total Oxidants	0.39	0.38	0.51	0.21
Observed F/mol Sulfur	0.60	0.59	0.78	0.33
Observed F/mol HgSO <sub>4</sub>	1.13	1.10	1.45	0.61
Watt Hours/in. 3 Net Cell	0.12	0.12	0.62	0.36
Terminal O. C. V. (at hours/V)	119/0.95	119/1.05	140/0.95	74/2.28

# Prismatic Configuration

# CODE

- c) Based on lighter load
- d) Based on heavier load
- q) Solid sheet

- v) Microporous Rubber
- w) Ag-plated Copper Exme
- x) Pure Silver Exmet
- y) Exmet

			E (		. 20
A 1 1 1	55	1 .	56	57	58
	extra anoc two edge:		MPR sealed	5- electrode research	Wt. ratio S:C = 5.7
Anodes Loaded		Anodes Loaded	at edges	cell. See text.	
0/1		10/13	34/40	25/57	53/89
	20		20	20	0
	4	•	4	4	21
	12		12	12	3.7
	0.020			0.020	0.020
			0.060		
16 <sup>q</sup>		21.0 <sup>q</sup>	210 <sup>q</sup>	105 <sup>q</sup>	210 <sup>q</sup>
$regular^q$		$edge^{q}$		1 <sup>q</sup> , 1 <sup>y</sup>	
210 <sup>w</sup>		210 <sup>w</sup>	210 <sup>w</sup>	105 <sup>w</sup>	210 <sup>w</sup>
	100		150	250	100
	7.5		10	17	7.5
	13.5/68		13.5/68	13.5/68	13.5/68
2.09		2.12	2. 25	2. 21	1.95
2.09		2.24	2. 27	2.24	1.98
1.30		1.30	1.30	1.30	1.30
2.05		2.04	1.52	1.67	1.82
6.32		0.75	0.78	1.46	0.62
		72	226	318	526
		0.09	0.29	0.41	0.17
		0.14	0.45	0.63	0.17
		0.27	0.83	1.18	
		0.11	0.27	0.22	0.67
		145/2.15	73/0.89		140/1.94

#### TABLE I

# ELECTROCHEMICAL CELL TESTS

Discharge Temperature: -90°C

Pasted Plate Configuration

Polyethylene Bag Vehicles

Cathode Collector: Silver-plated Exmet

Cathode Binder<sup>m</sup>: 0.2g Polystyrene in 20 cc Toluene for Std. 36g Cathodes Electrolyte: 34 Wt. % KSCN<sup>n</sup> in liquid ammonia

		· · · · · · · · · · · · · · · · · · ·		
Cell No. P-	59	60	61	62
Major Variables	Separation 7 layers		Thin Cathode	Separation 2 layers
Hours to End Voltage (1.5/1.3V)	24/26	55/56	73/82	40/64
Cathode: HgSO <sub>4</sub> <sup>j</sup> (g)	20	20	5.95	0
Cathode: Sulfur (g)	4 <sup>.</sup>	4	1.19	11.0
Cathode: Carbon (g)	12	12	3.57	11.0
Cathode: Paper Pulp (g)				
Separator Thickness (in.), M1365 <sup>u</sup>	0.028	0.028	0.020	0.008
Separator Thickness (in.), MPR			0.030	
Anode Area (cm²) AZ31B Mg	210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>9</sup>	210 <sup>q</sup>
Anode Reference AZ31B Mg	~			
Cathode Collector Area (cm²)	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>
Volume Electrolyte (cc)	100	100	100	100
Net Cell Volume (in.3)	7.5	7.5	7.5	7.5
Load <sup>a</sup> (ohms)	13.5/68	13.5/68	48/240	13.5/68
Initial Closed Circuit Voltage C	2.22	2. 22	2.20	1.94
Peak Closed Circuit Voltage	2.24	2. 24	2.20	2.00
End Voltage (heavy load)	1.30	1.30	1.30	1.30
End Voltage (light load)	2.08	2.01	1.50	1.80
Peak Current Density (mA/cm²)	0.75	0.75	0.22	0.64
Obs. Coulombs/g Total Oxidants	145	312	431	726
Observed F/mol Total Oxidants	0.19	0.40	0.56	0.24
Observed F/mol Sulfur	<sup></sup> 0.29	0.62	0.86	0.24
Observed F/mol HgSO <sub>4</sub>	0.54	1.15	1.59	
Watt Hours/in. 3 Net Cell	0.23	0.49	0.20	0.49
Terminal O.C.V. (at hours/V)	92/2.22	92/2.25	102/1.30	102/1.64

## Prismatic Configuration

# CODE

- c) Based on lighter load
- d) Based on heavier load
- q) Solid sheet

- v) Microporous Rubber
- w) Ag-plated Copper Exmet
- x) Pure Silver Exmet
- y) Exmet

63	65	66	69		70
Ag	Paste on of gr	id	3-Electrode	Cell	Single
Exmet Collector (x)	Paste facing anode	Grid facing anode	Sulfur electrode	Carbon l electrode	anode discharge
54/66	42/47	67/69	81/202	25	54/85
20	. 20	20	0	0	0
4	4 .	4	21	0	21
12	12	12	3.7	16	3.7
0.020	0.020	0.020	0.020	0.020	0.020
210 <sup>q</sup>	105 <sup>y</sup>	105 <sup>y</sup>	105 <sup>q</sup>	105 <sup>q</sup>	105 <sup>q</sup>
	(q)	(q <b>.</b> )			
210 <sup>x</sup>	105 <sup>w</sup>	105 <sup>w</sup>	105 <sup>w</sup>	105 <sup>w</sup>	105 <sup>w</sup>
150	150	150	150	150	150
10	10	10	10	10	10
13.5/68	13.5/68	13.5/68	13.5/O.C.	68	13.5/68
2. 21	2. 22	2. 22	1.61 <sup>d</sup>	1.41	1.85
2. 22	2.22	2.24	1.65 <sup>d</sup>	1.41	1.91
1.30	1.30	1.30	1.30		1.30
1.49	1.59	1.47	2.05 O.C.	0.65	1.77
0.77	1.51	1.52	1.16		1.14
366	260	385	377	64	490
0.47	0.34	0.50	0.13		0.16
0.73,	0.52	0.77	0.13		0.16
1.35	0.96	1.42			
0.43	0.30	0.45	0.32		0.46
73/1.73	74/1.47	74/1.47	311/2.03	311/1.82	237/1.19

# TABLE I ELECTROCHEMICAL CELL TESTS

Discharge Temperature: -90°C

Polyethylene Bag Vehicles

Pasted Plate Configuration

Cathode Collector: Silver-plated Exmet

Cathode Binder<sup>m</sup>: 0.2g Polystyrene in 20 cc Toluene for Std. 36g Cathodes Electrolyte: 34 Wt. % KSCN<sup>n</sup> in liquid ammonia

Call No. D	71	72	73	74	
Cell No. P-	/1	72	13	1.1	
Major Variables	1/4" Cath Single And Discharg	ode	5-electrode research cell. 3 cathodes.	Single Anode Ag Exmet collector (x)	
Hours to End Voltage (1.5/1.3V)	11/13	17/19	See text	4/27	
Cathode: HgSO <sub>4</sub> <sup>j</sup> (g)	40	40	0	0	
Cathode: Sulfur (g)	8	8	63	21	
Cathode: Carbon (g)	24	24	11.1	3.7	
Cathode: Paper Pulp (g)		0.72			
Separator Thickness (in.), M1365 <sup>u</sup>	0.020	0.020	0.020	0.020	
Separator Thickness (in.), MPR					
Anode Area (cm²) AZ31B Mg	105 <sup>q</sup>	105 <sup>q</sup>	105 <sup>q</sup>	105 <sup>q</sup>	
Anode Reference AZ31B Mg	(q)	(q)	<b>(</b> y <b>)</b>		
Cathode Collector Area (cm²)	105 <sup>w</sup>	105 <sup>w</sup>	315 <sup>w</sup>	105 <sup>x</sup>	
Volume Electrolyte (cc)	150	150	200	130	
Net Cell Volume (in.3)	10	10	21	9	
Load (ohms)	6.75/34	6.75/34	4.5/22.7	13.5/68	
Initial Closed Circuit Voltage	1.97	2.13	1.78	1.68	
Peak Closed Circuit Voltage C	2.00	2.18	1.90	1.83	
End Voltage (heavy load)	1.30	1.30	0.68	1.30	
End Voltage (light load)	1.90	1.78	1.61	1.76	
Peak Current Density (mA/cm <sup>2</sup> )	2.67	3.02	3.02	1.15	
Obs. Coulombs/g Total Oxidants	68	104		153	
Observed F/mol Total Oxidants	0.09	0.14		0.05	
Observed F/mol Sulfur	0.13	0.21		0.05	
Observed F/mol HgSO <sub>4</sub>	0.25	0.39			
Watt Hours/in. 3 Net Cell	0.15	0.24		0.16	
Terminal O.C.V. (at hours/V)	163/1.89	1.63/1.05	213/2.01	93/2.00	

# Prismatic Configuration

# CODE

- c) Based on lighter loadd) Based on heavier load
- q) Solid sheet

- v) Microporous Rubber
- w) Ag-plated Copper Exmet
- x) Pure Silver Exmet
- y) Exmet

75	76	77	.78	. 79	_
2-Anodes Ag Exmet	Sulfur	: Carbon Weig	ht Ratio:	· .	
collector (x)	2. 33	2. 33	1.50	1.50	
0/56	99/141	100/120	93/103	94/106	_
0	0	0	0	0	
21	17	17	14	14	
3.7	7.3	7.3	9.3	9.3	
0.020	0.020	0.020	0.020	0.020	
<b>~</b>			·		
210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>q</sup>	210 <sup>q</sup>	
	·				
210 <sup>x</sup>	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>	210 <sup>w</sup>	
130	125	125	125	125	
9	9	9	9	9	
13.5/68	13.5/68	13.5/68	13.5/68	13.5/68	
1.63	1.97	1.97	1.98	1.97	
1.80	1.99	1.99	2.00	2.00	
1.30	1, 30	1.30	1.30	1.30	
1.77	1.52	1.73	1.68	1.67	
0.49	0.70	0.70	0.70	0.70	
312	1035	882	918	945	
0.10	0.34	0.29	0.30	0.31	
0.10r	0.34	0.29	0.30	0.31	
0.31	0.90	0.77	0.65	0.67	
93/1.98	165/1.54	165/1.55	165/1.06	165/1.10	

#### TABLE I

#### ELECTROCHEMICAL CELL TESTS

Discharge Temperature: -90°C

Cathode Collector: Silver-plated Exmet W Polyethylene Bag Vehicles

Pasted Plate Configuration

Polyethyle
Cathode Binder

0.2g polystyrene in 20 cc toluene
M-1365 Separator: 5 layers at 0.004" per layer
Electrolyte: 34 Wt. % KSCN<sup>n</sup> in liquid ammonia

Cell No. P-	80	81	82	83	84
	Research	Acetylene Black			
Major Variables	Cell 3 Cath.	1500 6		30% Carbon	
	4 Anodes See Text.	15% C	arbon	30% 0	arbon
Hours to End Voltage (1.5/1.3V)	36/47	85/118	82/121	80/87	83/108
Cathode: Sulfur (g)	63	21	21	17	17
Cathode: Carbon (g)	11.1	3.3	2.9	6.6	5.9
Cathode: Acetylene Black (g)		0.4	0.8	0.7	1.4
Cathode: Paper Pulp (g)	w.,				
Anode Material: AZ31B Mg Sheet <sup>q</sup> Exmet <sup>y</sup>	1 q 3 y	2 <sup>q</sup>	2 <sup>q</sup>	2 <sup>q</sup>	2 <sup>q</sup>
Anode Area (cm²)	420	210	210	210	210
Cathode Collector <sup>w</sup> Area (cm²)	315	210	210	210	210
Volume Electrolyte (cc)	300	125	125	125	125
Net Cell Volume (in.3)	21	9	9	9	9
Load <sup>a</sup> (ohms)	4.5/22.7	13.5/68	13.5/68	13.5/68	13.5/68
Initial Closed Circuit Voltage c	1.93	1.99	1.94	1.98	2.04
Peak Closed Circuit Voltage c	1.95	2.09	2.08	2.03	2.09
End Voltage (Heavy Load)	1.30	1.30	1.30	1.30	1.30
End Voltage (Light Load)	1.82	1.77	1.71	1.70	1.62
Peak Current Density d (mA/cm²)	0.93	0.67	0.67	0.66	0.68
Observed Coulombs/g Sulfur	276	721	738	643	818
Observed F/mol Sulfur	0.09	0.24	0.24	0.21	0.27
Watt Hours/in.3 Net Cell	0.38	0.80	0.81	0.56	0.73
Terminal O.C.V. (at Hours/V)	167/1.85	146/1.82	146/1.70	146/1.50	146/1.55
Temperature °C Maximum	-89.1	-74.5	-74.5	-74.5	-74.5
Temperature °C Minimum	-90.2	-89.8	-898	-89.8	-89.8
Temperature °C (Time Weighted) Ave	· -89.7	-87.0	-87.0	-85.5	-88.8

# Prismatic Configuration

85	86	87	88	89	90	91	92	
	Paper Pu	lp		Acetylene Black				
30% Carbon		15% Carbon		15% Carbon		30% C	arbon	
75/89	72/109	68/100	45/69	44/72	76/85	52/80	81/86	
17	17	21	21	21	21	17	17	
7.3	7.3	3.7	3.7	3.3	2.9	6.6	5.9	
		:		0.4	0.8	0.7	1.4	
0.25	0.75	0.25	0.75					
2 <sup>q</sup>	2 <sup>q</sup>	2 <sup>q</sup>	2 <sup>q</sup>					
210	210	210	210	210	210	210	210	
210	210	210	210	210	210	210	210	
100	120	110	130	100	100	100	100	
7.5	8.5	8	9	7.5	7.5	7.5	7.5	
13.5/68	13.5/68	13.5/68	13.5/68	13.5/68	13.5/68	13.5/68	13.5/68	
1.95	1.94	1.92	1.91	1.90	1.94	1.94	1.99	
2.01	1.99	1.97	1.95	1.96	1.96	1.98	1.99	
1.30	1.30	1.30	1.30	1.30	1.30	1.30	1.30	
1.80	1.73	1.73	1.72	1.85	1.87	1.89	1.86	
0.63	0.64	0.62	0.60	0.60	0.62	0.62	0.65	
657	800	590	405	422	499	584	631	
0.22	0.27	0.20	0.13	0.14	0.17	0.19	0.21	
0.69	0.73	0.71	0.43	0.54	0.63	0.60	0.66	
136/1.80	,136/1.72	136/1.80	136/1.69	119/2.02	119/2.04	119/1.98	119/1.96	
-88.6	-88.6	-88.6	-88.6	-89.1	-89.1	-89.1	-89.1	
-90.9	-90.9	-90.9	-90.0	-90.8	-90.8	-90.8	-90.8	
-89.6	-89.7	-89.6	-89.2	-90.1	-90.1	-90.1	-90.1	

#### TABLE I

# ELECTROCHEMICAL CELL TESTS- Prismatic Configuration

Discharge Temperature: -90°C

Cathode Collector: Silver-plated Exmet W

Polyethylene Bag Vehicles

Pasted Plate Configuration Polyethyle Cathode Binder 20.2g polystyrene in 20 cc toluene

M-1365 Separator: 5 layers at 0.004" per layer Electrolyte: 34 Wt. % KSCN n in liquid ammonia

Cell No. P-	93	94	95	96	97
Major Variables	Research Cell 3 Cath. 6 Anodes See Text.	Single Disch 5-1/4" Holes in Anode		Replica Cells P-	
Hours to End Voltage (1.5/1.3V)	42/58	54/58	43/55	73/105	67/80
Cathode: Sulfur k (g)	63	17	17	17	17
Cathode: Carbon (g)	11.1	7.3	7.3	7.3	7.3
Cathode: Acetylene Black (g)					
Cathode: Paper Pulp (g)			· :		
Anode Material: AZ31B Mg Sheet <sup>q</sup> Exmet <sup>y</sup>	1 q 5 y	1 <sup>q</sup>	1 <sup>q</sup>	2 <sup>q</sup>	2 <sup>q</sup>
Anode Area (cm²)	630	105	105	210	210
Cathode Collector W Area (cm²)	315	105	105	210	210
Volume Electrolyte (cc)	300	100	100	100	100
Net Cell Volume (in.3)	21	7.5	7.5	7.5	7.5
Load a (ohms)	4.5/22.7	13.5/68	13.5/68	13.5/68	13.5/68
Initial Closed Circuit Voltage C	1.93	1.99	1.96	2.03	1.97
Peak Closed Circuit Voltage c	1.96	2.02	2.01	2.06	2.00
End Voltage (Heavy Load)	1.30	1.30	1.30	1.30	1.30
End Voltage (Light Load)	1.79	1.84	1.81	1.77	1.78
Peak Current Density d (mA/cm²)	0.62	1.30	1.30	0.67	0.66
Observed Coulombs/g Sulfur	340	428	405	785	587
Observed F/mol Sulfur	0.11	0.14	0.13	0.26	0.19
Watt Hours/in. Net Cell	0.46	0.45	0.42	0.83	0.61
Terminal O.C.V. (at Hours/V)		119/1.74	119/1.79	119/1.86	119/1.76
Temperature °C Maximum	-87.3	-79.8	-79.8	-79.8	-79.8
Temperature °C Minimum	-88.7	-88.5	-88.5	-88.5	-88.5
Temperature °C (Time Weighted) Ave	88.0	-84.5	-84. <b>8</b>	-84.4	-84. 4

TABLE I

#### ELECTROCHEMICAL CELL TESTS-

Cathode Binder: 0.2g polystyrene in 20 cc toluene Polyethylene Bag Vehicles M-1365 Separator: 5 layers at 0.004" per layer

Electrolyte: 34 wt. % KSCN<sup>n</sup> in liquid ammonia - 125 cc per cell

Anodes: AZ31B Mg Sheet<sup>q</sup>-2 per cell Area = 210 cm<sup>2</sup>

Cathode Collector Area =  $210 \text{ cm}^2$  Net Cell Volume =  $9 \text{ in.}^3$  Load  $(\Omega) = 13.5/68$ 

Nine 1/4" holes were drilled in the anodes of all cells, except P-100 and 101.

Cell No. P-	99	100	101		
Major Variables	-63°	-63°	-63°		
Wajor Variables	No holes in anodes Silver-plated copper Exmet collectors				
Hours to End Voltage (1.5/1.3V)	51/75	42/50	44/54		
Cathode: Sulfur k (g/%)	21/85	17/70	17/70		
Cathode: Carbon (g/%)	3.7/15	7.3/30	7.3/30		
Initial Closed Circuit Voltage	2.07	2.06	2.03		
Peak Closed Circuit Voltage	2.08	2.06	2.03		
End Voltage (Heavy Load)	1.30	1.30	1.30		
End Voltage (Light Load)	1.64	1.64	1.64		
Peak Current Density (mA/cm²)	0.70	0.70	0.69		
Observed Coulombs/g Sulfur	456	374	401		
Observed F/mol Sulfur	0.15	. 0.12	0.13		
Watt Hours/in. <sup>3</sup> Net Cell	0.50	0.33	0.35		
Terminal O. C. V. (at Hours/V)	116/1.54	89/1.52	89/1.56		
Temperature, °C (Maximum)	-64.0	-64.0	-64.0		
Temperature, °C (Minimum)	-66.2	-65.2	-65.2		
Temperature, °C (Time weighted Ave.)	<b>-</b> 65.1	-64.6	-64.6		
Residual Electrolyte Volume, %	90	90	50		
Corrosion of Collector	Severe	Severe	Moderate		
Elapsed Time, Hours	119	118	118		

# Prismatic Configuration

102	103	104	105	106	107	108	109
-63°	-63°	-63°	-63°	-63°	-63°	-63°	-40°
Silver-plated copper Exmet collectors			Pb Exmet (	Collector	Perforated Al Collectors		
66/75	38/48	28/49	49/75	42/54	37/56	0/0	0/0
17/70	17/70	17/70	21/85	17/70	17/70	21/85	21/85
<b>7</b> .3/30	7.3/30	7.3/30	3.7/15	7.3/30	7.3/30	3.7/15	3.7/15
2.11	2.08	2.06	2.06	1.75	1.79	1.21	1.43
2.12	2.08	2.07	2.06	1.75	1.79	1.21	1.56
1.30	1.30	1.30	1.30	1.30	1.30	0.81	1.07
1.58	1.66	1.75	1.64	1.69	1.68		1.46
0.71	0.71	0.70	0.70	0.60	0.61		
571	361	367	454	367	386		
0.19	0.12	0.12	0.15	0.12	0.13		
0.51	0.32	0.33	0.50	0.30	0.31		~
89/1:.60	116/1.55	116/1.58	116/1 53	91/1.71	91/1.77	17/2.00	66/1.78
-64.0	-64.0	-64.0	-64.0	-64.0	-64.0	-63.0	~-~
-65.2	-65.3	<b>-</b> 65.3	-66.2	-65.3	-65.3	-65.3	
-64.7	-64.9	-64.8	-65.1	-64.8	-64.8	-64.5	-40
40	40	60	90	75	75	50	Wet, only
Moderate	Severe	Severe	Severe	Destroyed	Destroyed	None	Nil
118	120	120	119	95	95	48	94

ELECTROCHEMICAL CELL TESTS-

TABLE I

Cathode Binder<sup>m</sup>: 0.2g polystyrene in 20 cc toluene Polyethylene Bag Vehicles M-1365 Separator: 5 layers at 0.004" per layer Electrolyte: 34 wt. % KSCN<sup>n</sup> in liquid ammonia - 125 cc per cell Anodes: AZ31B Mg Sheet<sup>q</sup>-2 per cell Area = 210 cm<sup>2</sup>

Cathode Collector Area =  $210 \text{ cm}^2$  Net Cell Volume =  $9 \text{ in.}^3$  Load  $(\Omega) = 13.5/68$ Nine 1/4" holes were drilled in the anodes of all cells, except P-100 and 101.

Cell No. P-	110	111
	-63°	-40°
Major Variables	Perforated A	luminum Collectors yy
Hours to End Voltage (1.5/1.3V)	15/44	13/37
Cathode: Sulfur k (g/%)	17/70	17/70
Cathode: Carbon (g/%)	7.3/30	7.3/30
Initial Closed Circuit Voltage <sup>C</sup>	1.87	2.06
Peak Closed Circuit Voltage	1.89	2.09
End Voltage (Heavy Load)	1.30	1.30
End Voltage (Light Load)	1.75	1.77
Peak Current Density (mA/cm²)	0.57	0.61
Observed Coulombs/g Sulfur	313	280
Observed F/mol Sulfur	0.10	0.09
Watt Hours/in. <sup>3</sup> Net Cell	0.26	0.25
Terminal O. C. V. (at Hours/V)	47/1.96	66/1.83
Temperature, °C (Maximum)	<b>-63.0</b>	
Temperature, °C (Minimum)	-65.3	
Temperature, °C (Time weighted Ave.)	-64.5	-40
Residual Electrolyte Volume, %	60	Wet, only
Corrosion of Collector	None	Nil
Elapsed Time, Hours	48	94

Continued

Prismatic Configuration

 			<del></del>		
 112	113	114	115	116	117
-63°	-63°	-40°	-40°	-40°	-40°
Gold-plated	d Copper E	Exmet Coll	ectors	Ag-plated C	u Collectors <sup>w</sup>
64/75	65/73	38/52	34/39	8/11	30/35
- <del></del>					
17/70	17/70	17/70	17/70	17/70	17/70
7.3/30	7.3/30	7.3/30	7.3/30	7.3/30	7.3/30
 2.06	2.05	2.15	2.14	2.05	2.10
2.07	2.07	2.15	2.14	2.05	2.11
1.30	1.30	1.30	1.30	1.30	1.30
1.55	1.83	1.82	1.72	1.46	1.57
 0.67	0.67	0.73	0.72	0.69	0.72
567	552	400	2.98	82	274
0.19	0.18	0.13	0.10	0.03	0.09
0.51	0.49	0.36	0.27	0.07	0.25
 87/1.86	87/1.94	66/2.05	66/2.00	66/1.57	66/1.60
-64.5	-64.5				
-65.7	-65.7				
-64.8	-64.8	-40	-40	-40	-40
 80	75	20	20	80	80
Nil	Nil	Nil	Mild	Severe	Severe
114	114	95	95	96	96

## TABLE I

## ELECTROCHEMICAL CELL TESTS-

Polyethylene Bag Vehicles

Anode Area (2 sides): 210 cm<sup>2</sup> Thickness: 0.016" AZ31B Mg Sheet<sup>q</sup>

Cathode Collector Area (2 sides): 210 cm<sup>2</sup>

Cathode Binder : 0.2g polystyrene in 20 cc toluene M-1365 Separator : 5 layers at 0.004" per layer Load  $^{a}(\Omega) = 13.5/68$ 119 120 121 Cell No. P-118 Nominal Discharge Temp. (°C) **-**63 -40 -63 -40

Major Variables	Temperature Cathode Compos.		Tempera Cathode	
Hours to End Voltage (1.5/1.3V)	32/38	35/39	35/51	29/38
Cathode: HgSO <sub>4</sub> <sup>j</sup> (g/%) Sulfur <sup>k</sup> (g/%) Carbon <sup>l</sup> (g/%) Collector	20/55.6 4/11.1 12/33.3 w	20/55.6 4/11.1 12/33.3 w		20/55.6 4/11.1 12/33.3 w
Electrolyte: KSCN <sup>nn</sup> (% as KSCN)  Mg(SCN) <sub>2</sub> (% as KSCN)  "Spent" (% as KSCN)  Volume (cc)	34 125	34 125	34 125	34 125
Net Cell Volume (in.3)	9	9	9	9
Initial Closed Circuit Voltage <sup>C</sup> Peak Closed Circuit Voltage <sup>C</sup> End Voltage (Heavy Load) End Voltage (Light Load)	2.13 2.13 1.30 1.52	2. 24 2. 24 1. 30 1. 40	2. 27 2. 32 1. 30 1. 47	2. 25 2. 31 1. 30 1. 39
Peak Current Density d (mA/cm²) Observed Coulombs/g Total Oxidants Observed F/mol Total Oxidants Observed F/mol Sulfur Observed F/mol HgSO <sub>4</sub> Watt Hours/in. 3 Net Cell	0.73 206 0.27 0.41 0.76 0.26	0.77 218 0.28 0.43 0.80 0.29	0.80 291 0.38 0.58 1.08 0.39	0.80 217 0.28 0.43 0.80 0.29
Terminal O. C. V. (at Hrs./V)	67/1.07	67/0.75	67/1.41	67/1.03

## Prismatic Configuration

125	126	127	128	129	130
-63	-90	-90	-90	-90	-63
Note 1	Virgin Ele Cathode C	-	"Spent" El Cathode (	•	Temperature Conc. of Electrolyte
41/43	0/95	17/89	25/110	90/113	25/30
20/55.6 4/11.1 12/33.3 zz	0 21/85 3.7/15 w	0 21/85 3.7/15 w	0 17/70 7.3/30 w	0 17/70 7.3/30 w	20/55.6 4/11.1 12/33.3 w
25	25	25			25
125 9	200 13	200 13	25 200 13	25 200 13	125 9
2. 23 2. 24 1. 30 1. 54	1.78 1.84 1.30 1.74	1.81 1.86 1.30 1.76	1.83 1.89 1.30 1.71	1.76 1.86 1.30 1.71	1.98 1.98 1.30 1.50
0.77 240 0.31 0.48 0.89 0.32	0.53 538 0.18 0.18  0.38	0.57 506 0.17 0.17  0.36	0.55 782 0.26 0.26  0.45	0.54 794 0.26 0.26  0.46	0.67 155 0.20 0.31 0.57
65/0.85	137/1.82	137/1.78	210/1.35	210/1.34	65/1.08

<sup>&</sup>lt;sup>1</sup> Electrolyte Concentration, Aluminum Exmet Collector.

## TABLE I (Continued)

## ELECTROCHEMICAL CELL TESTS - Prismatic Configuration

Polyethylene Bag Vehicles

Anode Area (2 sides): 210 cm<sup>2</sup> Thickness: 0.016" AZ31B Mg Sheet<sup>q</sup>

Cathode Collector Area (2 sides): 210 cm<sup>2</sup>

Cathode Binder<sup>m</sup>: 0.2g polystyrene in 20 cc toluene Load<sup>a</sup>  $(\Omega) = 13.5/68$ M-1365 Separator<sup>u</sup>: 5 layers at 0.004" per layer Cell No. P-131 132 133 134 Nominal Discharge Temp. °C -63 -63 -90 -90 Electrolyte Conc.  $Mg(SCN)_2$ Each anode loaded Al Exmet collec-Electroseparately with 1/2 usual load. Major Variables tor. lyte - S treatment. Anode Anode В Α Hours to End Voltage (1.5/1.3V) 45/82 57/83 0/12 69/110 71/113 Cathode: HgSO<sub>4</sub>, 0 0 0 0 Sulfur (g/%)Carbon (g/%)17/70 17/70 17/70 17/70 7.3/30 7.3/30 7.3/307.3/30Collector zzzzw Electrolyte: KSCN<sup>nn</sup> (% as KSCN) 25 25 34 Mg(SCN)<sub>2</sub> (% as KSCN) 34 \_ \_ \_ (% as KSCN) "Spent" \_\_\_ ---Volume (cc) 125 125 125 125 Net Cell Volume (in.3) 9 9 Initial Closed Circuit Voltage 2.05 2.05 1.64 1.87 1.82 Peak Closed Circuit Voltage 1.91 1.88 2.05 2.05 1.71 End Voltage (heavy load) 1.30 1.30 1.30 1.30 1.30 End Voltage (light load) 1.75 1.79 1.65 1.69 1.53 Peak Current Density (mA/cm²) 0.63 0.64 0.65 0.48 0.62 Observed Coulombs/g Total Oxidants 620 392 399 612 80 Observed F/mol Total Oxidants 0.20 0.20 0.03 0.13 0.13 Observed F/mol Sulfur 0.13 0.20 0.20 0.03 0.13 Observed F/mol HgSO4 ---------\_ \_ \_ Watt Hours/in. 3 Net Cell 0.33 0.33 0.54 0.55 0.06 Terminal OCV (at hrs. /V)

162/1.70 162/1.73 257/0.62

## TABLE II

## ELECTROCHEMICAL CELL TESTS-

Temperature (Time Weighted) Average

y) AZ31B Mg Exmet
 u) M-1365 Separator - 5 layers at 0.004" per layer = 0.020" thick Electrolyte: 34 Wt. %KSCN<sup>n</sup> in liquid ammonia

Cell No. B-	1	2	3	
Major Variables	Inverse Bobbins Porous polyethylene M-1365 u			
Wajor variables	Porous polye		-	
	Separators Z	tral rod anode	Separation	
	Cen	itrai rod anode	S	
Hours to End Voltage (1.5/1.3V)	2/4	0/0	0/0	
Cathode: HgSO <sub>4</sub> (grams/%) Cathode: Sulfur (grams/%)	100/55.6	0	0	
Cathode: Sulfur (grams/%)	20/11.1	102/85	42.5/70	
Cathode: Carbon (grams/%)	60/33.3	18/15	18.2/30	
Cathode: Acetylene Black				
Cathode Thickness (in.)	0.45	0.45	0.35	
Cathode Length (in.)	5.5	4.5	5.0	
Cathode Collector, Ag Wire (W) or Case (C)	2W	2W .	1W, 1C	
Anode, Central (Cylindrical)	${f Mg} \; {f rod}^{f I}$	${f Mg\ rod}^{f I}$	Mg rod <sup>g</sup>	
Apparent Area (cm²)	56	46	51	
Anode, Outer (Cylindrical)				
Apparent Area (cm²)				
Net Cell Volume (in.3)	16	16	12	
Load (ohms)	2.7/13.5	2.7/13.5	5. 4/27	
Initial Closed Circuit Voltage	2.10	0.70	1.52	
Peak Closed Circuit Voltage	2.11	0.73	1.52	
End Voltage (Heavy Load)	1.30			
End Voltage (Light Load)	2.08			
Peak Anode Current Density (mA/cm²) <sup>d, e</sup>	10.8	Nil	2.3	
Obs. Coulombs/g Total Oxidants	Nil	IVII	Nil	
Observed F/mol Total Oxidants	Nil		INII	
Observed F/mol Sulfur	1411			
Observed F/mol HgSO <sub>4</sub>				
Watt Hours/in. 3 Net Cell				
Terminal OCV (at Hours/V)	116/2.30	116/2.10	78/2.18	
Temperature (°C) Marinum	-89.0	-89.0		
Temperature (°C) Maximum Temperature (°C) Minimum	-99.9	-89.0 -90.9		
Temperature ( C) withinum	70.7	-70.7		

-90.0

-90.0

-89.8

## Bobbin Configurations - Nominal Minus 90°C

• <u>-</u>	4	5	6	7
	Inve	rse Bobbins		Holes in Anodes
	N	1-1365 Separation <sup>u</sup>		
		Coiled C	entral Exmet Anodes	
	Acetylene	MPR <sup>v</sup> spacer	Larger	Added outer
	Black	in anode coil	Diam. anode	anodes
	22/28	20/31	32/35	50/70
	0	0	0	0
	42.5/70	85.0/70	70.8/70	47.6/70
	12.1/20	36.4/30	30.3/30	20.4/30
	6.1/10		·	
	0.32	0.37	0.27	0.24
	6.0	5 <b>.0</b>	5.0	5.3
	1 C	1 C	1 C	4W
	Coil y	Coil <sup>y</sup>	Coil <sup>y</sup>	Coil y
	99	114	133	108
				3 sheets <sup>y</sup>
				167
	17	25	25	27
	5.4/27	5.4/27	5.4/27	5.4/27
	2.03	1.99	2.03	2. 02
	2.03	1.99	2.05	2.02
	1.30	1.30	1.30	1.30
	1.85	1.87	1.87	1.80
<del></del>				
	3. 25	2.65	2.50	1.21
	208	114	157	461
	0.07	0.04	0.05	0.15
	0.07	0.04	0.05	0.15
	 0.24	0.10	0.21	0.39
	145/2.10	0.18	150/2.06	0.38 70/2.09
				,
	-89.2	-87.8	-87.8	-79.5
	-90.7	-88.6	-89.0	-86.3
	-89.7	<b>-</b> 88.5	-88.2	<b>-84</b> .1

## TABLE II

## ELECTROCHEMICAL CELL TESTS

Bobbin Configurations - Nominal -90°C

q) AZ31B Mg Sheet. u) M-1365 Separator, 5 layers at 0.004" per layer = 0.020" thick. y) AZ31B Mg Exmet. Electrolyte: 34 Wt. % KSCN<sup>n</sup> in liquid ammonia

Cell No. B-	81	91
Major Variables	Annular R Cathode	0
	Exmet Anodes	Sheet Anodes
Hours to End Voltage (1.5/1.3V)	18/42	10/21
Cathode: Sulfur (grams/%)	47.6/70	47.6/70
Carbon <sup>l</sup> (grams/%)	20.4/30	20.4/30
Cathode Thickness (in.)	0.24	0.25
Cathode Length (in.)	7	5.5
Cathode Collector: Ag Wire (W) or Case (C)	4 W	4W
Anode: Central (Cylindrical)	Coily	Coil <sup>q</sup>
Apparent Area (cm²)	144	120
Anode: Outer (Cylindrical)	2 sheets <sup>y</sup>	2 sheets <sup>q</sup>
Apparent Area (cm²)	226	188
Net Cell Volume (in.3)	27	23
Load <sup>a</sup> (Ω)	5.4/27	5.4/27
Initial Closed Circuit Voltage	1.76	1.75
Peak Closed Circuit Voltage C	1.82	1.84
End Voltage (heavy load)	1.30	1.30
End Voltage (light load)	1.67	1.70
Peak Anode Current Density (mA/cm <sup>2</sup> ) <sup>d, e</sup>	0.77	0.92
Observed Coulombs/g Sulfur	260	130
Observed F/mol Sulfur	0.09	0.04
Watt Hours/in. 3 Net Cell	0.20	0.12
Terminal OCV (at hours/V)	65/2.02	65/2.02
Temperature (°C) Maximum	-66.0	-66.0
Temperature (°C) Minimum	-90.0	-90.0
Temperature (Time Weighted) Average	-81.5	-81.0

<sup>&</sup>lt;sup>1</sup> Design similar to B-7, except both central and outside anode layers were separated <sup>2</sup> Two (2) outer anodes separated by MPR strips. 1/4" holes in anodes.

<sup>3</sup> Ln. = Longitudinal

102	112	12	
Central Bol Cathodes	bbin	Central Anode 6 Ln. <sup>3</sup> Fins	
Exmet Anodes	Sheet Anodes	Annular Ring Cathode	
1/18	0/0	19/26	
84/70	84/70	84/70	
36/30	36/30	36/30	
1.16	1.16	0.37	
7.3	7.5	5.5	
2W	2W	1 C	
		$\mathtt{Fins}^{\mathtt{q}}$	
with seaso and		186	
2 sheets <sup>y</sup>	2 sheets <sup>q</sup>		
175	181		
27	27	23	
2.7/13.5	2.7/13.5	5.4/27	
1.64	1.69	1.73	
1.68	1.70	1.90	
1.30	1.29	1.30	
1.64	1.65	1.70	
2.79	2.66	1.59	
121		94	
0.04		0.03	
0.16		0.15	
65/2.00	65/2.03	65/2.00	
-66.0		-66.0	
-90.0		-90.0	
-81.0	-90.0	-81.8	

by MPR strips. 1/4" holes in anodes.

TABLE II

ELECTROCHEMICAL CELL TESTS-

Nominal Discharge Temperature: -90°C (Except B-22)
AZ31B Mg Sheet AZ31B Mg Exmet
M-1365 Separator Slayers at 0.004" per layer

Cell No. B-	13	14
Major Variables	Central & outside anodes. Annular ring cathode.	2 outside anodes central behalf
Hours to End Voltage (1.5/1.3V)	23/56	0/22
Cathode: HgSO <sub>4k</sub> (grams/%)	0	0
Sulfur, (grams/%)	63/70	98/7©
Carbon (grams/%)	27/30	42/30
Acetylene Black (grams/%)	0	0
Thickness (in.)	0.24	1.16
Length (in.)	6.75	10
Collector: Ag Wire (W) or Case (C)	4W	2W
Anode: Central (Cylindrical)	Coil y	
Apparent Area (cm <sup>2</sup> )	139	~
Outer (Cylindrical)	2 sheets <sup>y</sup>	2 sheets <sup>y</sup>
Apparent Area (cm²)	218	242
Electrolyte: KSCN <sup>nn</sup> (Wt. % as KSCN)	34	34
Mg(SCN) <sub>2</sub> (Wt. % as KSCN)		
"Spent" (Wt. % as KSCN)		
Volume (cc)	400	500
Net Cell Volume (in.3)	27	35
$Load^a(\Omega)$	5.4/27	2.7/13.5
Initial Closed Circuit Voltage	1.84	1.77
Peak Closed Circuit Voltage	1.84	1.80
End Voltage (Heavy Load)	1.30	1.30
End Voltage (Light Load)	1.78	1.71
Peak Current Density (mA/cm²) <sup>d, e</sup>	0.79	2.14
Observed Coulombs/g Sulfur	264	132
Observed F/mol Sulfur	0.09	0.04
Watt Hours/in. Net Cell	0.27	0.15
Terminal O. C. V. (at Hours/V)	67/2.08	45/1.96

Bobbin Configurations

15	16	17	19	20	21
Central	Central				
anode.	Exmet		''Spent''		
10 Longi-	coil + 3	''Spent''	Electrolyte		
tudinal	outer	Electro-	Acet. Black	Mg(SCN) <sub>2</sub> B	
fins.	anodes.	lyte		S: C	HgSO <sub>4</sub> :C
54/62	25/42	36/63	80/91	2/6	1/3
0	0	0	0	0	110/55.6
84/70	61.6/70	84/70	44.4/50	44.4/50	22/11.1
36/30	26.4/30	36/30	40.0/45	40.0/45	66/33.3
)	0	0	4.4/5	4.4/5	0
0.30	0.25	0.30	0.30	0.30	0.30
6.75	5.25	6.75	6.75	6.75	6.50
l C	4 W	1 C	1 C	1 C	1 C
l0 Fins <sup>q</sup>	Coily	10 Fins <sup>q</sup>	10 Fins <sup>q</sup>	10 Fins q	10 Fins q
171	108	171	171	171	165
	3 sheets <sup>y</sup>				
	167				
34	34				
·				24.5	24.5
		25	25		
100	350	400	350	400	300
31	27	31	28	31	25
5.4/27	5.4/27	5.4/27	5.4/27	5.4/27	5.4/27
1.93	1.91	1.91	1.92	1.94	2.01
l. 9 <b>4</b>	1.91	1.91	1.92	1.94	2.01
1.30	1.30	1.30	1.30	1.30	1.30
1.82	1.84	1.83	1.79	1.76	1.95
. 78	1.06	1.79	1.83	1.74	1.81
226	209	228	624	41	
0.08	0.07	0.08	0.21	0.01	
0.28	0.21	0.28	0.44	0.03	
67/2.13	47/2.13	89/2.08	93/2.06	18/2.08	17/2.12
<del></del>					

TABLE II

## ELECTROCHEMICAL CELL TESTS-

155/2.13

Nominal Discharge Temperature: -90°C (Except AZ31B Mg Sheet AZ31B Mg Exmet M-1365 Separator 1 5 layers at 0.004" per layer		
Cell No. B-	22	
Major Variables	1/2 Virgin + 1 electrolyte -40°C (+)	-63°C
		Cumulative Hours
Hours to End Voltage (1.5/1.3V)	26/30	59/72
Cathode: HgSO <sub>4k</sub> (grams/%) Sulfur (grams/%) Carbon (grams/%) Acetylene Black (grams/%) Thickness (in.) Length (in.) Collector: Ag Wire (W) or Case (C)  Anode: Central (Cylindrical) Apparent Area (cm²) Outer (Cylindrical)	0 44.4 40.0 4.4/ 0.30 6.25 1C 10 F 158	/50 /45 5
Apparent Area (cm²)  Electrolyte: KSCN <sup>nn</sup> (Wt. % as KSCN)  Mg(SCN) <sub>2</sub> (Wt. % as KSCN)  "Spent" (Wt. % as KSCN)  Volume (cc)	25  25 450	
Net Cell Volume (in.3)	33	
Load <sup>a</sup> (Ω) Initial Closed Circuit Voltage <sup>c</sup> Peak Closed Circuit Voltage End Voltage (Heavy Load) End Voltage (Light Load)	5.4/ 2.15 2.16 1.30 1.84	2.02 2.02 2.02 1.30 1.89
Peak Current Density (mA/cm²) <sup>d</sup> , e Observed Coulombs/g Sulfur Observed F/mol Sulfur Watt Hours/in. Net Cell	2.37 221 0.07 0.14	1.93 297 0.10 0.18

Terminal O. C. V. (at Hours/V)

## Bobbin Configuration

			<del></del>	
23	24	25	26	27
Electrolyte	1/2 Virgin +			Ball-milled
conc. & kind	1/2 "Spent"	S:C ratio	Ball-milled	in heptane
Acet. Black	electrolyte	No Acet. Black	in heptane	Electrolyte
				concentration
66/73	71/84	51/51	56/67	40/47
0	0	0	0	0
44.4/50	44.4/50	44.4/50	45.0/50	45.0/50
40.0/45	40.0/45	44.4/50	40.5/45	40.5/45
4.4/5	4.4/5	0	4.5/5	4.5/5
0.30	0.30	0.30	0.30	0.30
6.75	6.75	6.75	6.75	6.75
1C	1C	1 C	1C	1C
10 Fins q	10 Fins <sup>q</sup>	10 Fins <sup>q</sup>	10 Fins <sup>q</sup>	10 Fins <sup>q</sup>
171	171	171	171	171
	~			
34	25	34	34	25
	25			
400	400	400	400	400
31	31	31	31	31
5.4/27	5.4/27	5.4/27	5.4/27	5.4/27
1.95	1.91	1.95	1.91	1.99
1.95	1.99	1.95	1.94	1.99
1.30	1.30	1.30	1.30	1.30
1.78	1.81	1.88	1.71	1.82
1.86	1.81	1.82	1.83	1.84
507	590	354	456	326
0.17	0.20	0.12	0.15	0.11
0.33	0.39	0.23	0.30	0.22
117/2.09	225/1.85	117/2.01	136/1.96	87/2.09

TABLE II

## ELECTROCHEMICAL CELL TESTS-

Nominal Discharge Temperature: -90°C (Except AZ31B Mg Sheet AZ31B Mg Exmet M-1365 Separator: 5 layers at 0.004" per layer		
Cell No. B-	28	29
Major Variables	Full sized cell. 20% Acet. Black	90% KSCN + 10% Mg(SCN) <sub>2</sub> 20% Acet. Black
Hours to End Voltage (1.5/1.3V)	53/57	30/41
Cathode: HgSO <sub>4k</sub> (grams/%) Sulfur (grams/%) Carbon (grams/%) Acetylene Black (grams/%) Thickness (in.) Length (in.) Collector: Ag Wire (W) or Case (C)  Anode: Central (Cylindrical) Apparent Area (cm²) Outer (Cylindrical) Apparent Area (cm²)  Electrolyte: KSCN <sup>fm</sup> (Wt. % as KSCN) Mg(SCN) <sub>2</sub> (Wt. % as KSCN) "Spent" (Wt. % as KSCN) Volume (cc)	0 81.0/50 48.5/30 32.5/20 0.30 13.5 1C  10 Fins q 342 575	0 50/50 30/30 20/20 0.30 6.75 1C  10 Fins <sup>q</sup> 171 25 25 25
Net Cell Volume (in.3)	48	34
Load <sup>a</sup> (\Omega) Initial Closed Circuit Voltage <sup>c</sup> Peak Closed Circuit Voltage End Voltage (Heavy Load) End Voltage (Light Load)	2.7/13.5 1.94 1.95 1.30 1.82	5.4/27 2.01 2.01 1.30 1.82
Peak Current Density (mA/cm <sup>2</sup> ) <sup>d</sup> , e Observed Coulombs/g Sulfur Observed F/mol Sulfur Watt Hours/in. <sup>3</sup> Net Cell	1.85 431 <b>0.14</b> 0.33	1.89 257 0.09 0.17

Terminal O. C. V. (at Hours/V)

112/2.09

42/2.11

## Bobbin Configuration

30	31	32
10% Acet. Black	Electrolyte concentration	50% Acet. Black No graphite Mixed in heptane and dried
68/76	43/53	67/75
0 kk 48/50 kk 38/40 10/10 0.30 5.75	0 48/50 38/40 10/10 0.30 6.75	0 35/50 <sup>kk</sup> 0 35/50 0.30 6.75
10 Fins <sup>q</sup> 171 	10 Fins <sup>q</sup> 171	10 Fins <sup>q</sup> 171
34  350	25  400	34  400
28	31	31
5.4/27 2.01 2.01 1.30 1.79	5.4/27 2.06 2.06 1.30 1.82	5.4/27 2.01 2.01 1.30 1.75
1.93 498 0.17 0.39	1.99 352 0.12 0.25	1.88 674 0.22 0.35
87/2.05	87/2.08	117/1.79

TABLE II

ELECTROCHEMICAL CELL TESTS - Bobbin Configurations

Nominal Discharge Temp.: -90°C (except B-38, -39, -40, -41, -48, -49, -56) M-1365 Separator: 5 layers at 0.004" per layer
Case served as cathode collector. Electrolyte: 34 Wt. % KSCN<sup>nn</sup>, except B-56) Central finned anode (10 fins q), AZ31B Mg Sheet.

Cell No. B-	33	34	35	36	37
Major Variables	Cells B-3	33 to B-40	were packe	ed with a r	od, as usual.
Hours to End Voltage (1.5/1.3V)	56/63	61/70	48/53	51/56	54/63
Cathode: Sulfur kk (grams/%)	85/50	Replicat	tes of Cell	B-33.	
Carbon <sup>1</sup> (grams/%)	68/40				
Acetylene Black (g/%)	17/10			•	
Total Weight (grams)	170				
Cathode Thickness (inches)	0.30				
Cathode Length (inches)	13.5				
Anode: Apparent Area (cm²)	342				
Electrolyte Volume (cc)	660	660	660	660	660
Net Cell Volume (inches <sup>3</sup> )	53	53	53	53	53
Load <sup>a</sup> (ohms)	2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5
Initial Closed Circuit Voltage <sup>C</sup>	1.94	1.96	1.95	1.93	1.95
Peak Closed Circuit Voltage c	1.97	1.99	1.97	1.95	1.96
End Voltage (Heavy Load)	1.30	1.30	1.30	1.30	1.30
End Voltage (Light Load)	1.81	1.80	1.78	1.76	1.80
Peak Current Density (mA/cm <sup>2</sup> ) <sup>d, 6</sup>	1.86	1.90	1.87	1.87	1.88
Observed Coulombs/g Sulfur	459	514	387	407	<b>4</b> 59
Observed F/mol Sulfur	0.15	0.17	0.13	0.14	0.15
Watt Hours/inches Net Cell	0.34	0.38	0.28	0.29	0.34
Terminal O.C.V. (at Hours/V)	71/2.12	71/2.10	71/2.12	71/2.09	71/2.11

38	39	40	41	42					
-63°	-63°	-40°	-40°						
Cells B-33 a rod, as u	to B-40 were p sual.	acked with		Cells B-41 to B-64 were packed with an annular sleeve piston					
59/73	47/61	83/100	99/108	49/61					
42.5/50	48/50	48/50	48/50	120/50					
34.0/40	38.5/40	38.5/40	38.5/40	96/40					
8.5/10	9.5/10	9.5/10	9.5/10	24/10					
85	96	96	96	240					
0.30	0.30	0.30	0.30	0.30					
6.75	6.75	6.75	6.75	13.5					
171	171	171	171	342					
450	450	440	460	690					
34	34	34	34	55					
5.4/27	5.4/27	5.4/27	5.4/27	2.7/13.5					
2.08	2.09	2.16	2.16	1.97					
2.10	2.10	2.16	2.15	1.97					
1.30	1.30	1.30	1.30	1.30					
1.82	1.57	1.97	1.95	1.80					
2.04	2.06	2.19	2.18	1.88					
551	408	681	736	314					
0.18	0.14	0.23	0.24	0.10					
0.33	0.27	0.46	0.50	0.30					
140/1.76	140/1.56	115/2.06	115/2.04	68/2.08					

TABLE II

## ELECTROCHEMICAL CELL TESTS - BOBBIN CONFIGURATIONS

Nominal Discharge Temp.: -90°C (except B-38, -39, -40, -41, -48,

M-1365 Separator<sup>u</sup>: 5 layers at 0.004" per layer

Case served as cathode collector. Electrolyte: 34 Wt. % KSCN nn

Central finned anode (10 fins<sup>q</sup>), AZ31B Mg Sheet.

Cell No. B-	43	44	45	46	47					
Major Variables	Cells B-41 to B-64 were packed with an annular sleeve piston									
Hours to End Voltage (1.5/1.3V)	55/77	52/58	57/65	52/58	55/63					
Cathode: Sulfur (grams/%)	96/50	Replicate	es of Cell	B-43						
Carbon (grams/%)	77/40									
Acetylene Black (g/%)	19/10									
Total Weight (grams)	192									
Cathode Thickness (inches)	0.30									
Cathode Length (inches)	13.5									
Anode: q Apparent Area (cm²)	342									
Electrolyte Volume (cc)	690	690	670	710	690					
Net Cell Volume (inches3)	55	55	55	55	.55					
Load <sup>a</sup> (ohms)	2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5					
Initial Closed Circuit Voltage c	1.96	1.96	1.95	1.96	1.94					
Peak Closed Circuit Voltage C	1.96	1.98	1.96	1.97	1.94					
End Voltage (Heavy Load)	1.30	1.30	1.30	1.30	1.30					
End Voltage (Light Load)	1.80	1.79	1.77	1.77	1.77					
Peak Current Density (mA/cm <sup>2</sup> ) <sup>d, e</sup>	1.89	1.85	1.85	1.86	1.86					
Observed Coulombs/g Sulfur	495	375	419	375	403					
Observed F/mol Sulfur	0.16	0.12	0.14	0.12	0.13					
Watt Hours/inches Net Cell	0.39	0.30	0.33	0.30	0.32					
Terminal O.C, V. (at Hours/V)	89/2.10	113/2.07	113/2.07	113/1.94	113/2.03					
No. of Hose Clamps	6	4	4	4	4					

-49, -56)

except	B-56)
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48	49	50	51	52						
	Cu Exmet									
7 collector clamps on	sleeve on	sleeve on case secured Replicates of B-49								
case.	by 14 clamps.	-	rect at -90°C	S: C Ratio						
Temp. Note l	Temp. Note 2	·	· · · · · · · · · · · · · · · · · · ·							
67/116	47/127	56/61	62/69	61/68						
Replicates	s of Cell B-43, exce	pt for means	of	77/40						
collection	from case.	aller ann mar mar mar ann ann ann ann an ann ann ann ann an	· · · · · · · · · · · · · · · · · · ·	96/50						
				19/10						
				192						
				0.30						
				13.5						
				342						
575	700	650	650	650						
55	55	55	55	55						
2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5	2.7/13.5						
1.95	1.94	1.99	1.98	1.98						
2.08	2.14	1.99	1.98	1.98						
1.30	1.30	1.30	1.30	1.30						
1.85	1.85	1.79	1.80	1.81						
2. 06	2.18	1.96	1.91	1.91						
772	862	397	449	548						
). 26	0.29	0.13	0.15	0.18						
0.63	0.72	0.32	0.36	0.35						
142/2.06	138/2.01	119/2.00	118/2.07	118/2.05						
1 + 3	14	15	18	16						

Double lead wires from cells to loads used on Cells B-49 to B-56, except B-54 Note 1 - Temp.: 24 hours at -90°; 20 hours from -90° to -55°; balance of test at -65°C.

Note 2 - Temp.: 18 hours from -90° to -51°; balance at -65°C.

## TABLE II

## ELECTROCHEMICAL CELL TESTS - BOBBIN CONFIGURATIONS

Nominal Discharge Temp.: -90°C (except B-38, -39, -40, -41, -48, -49, -56 M-1365 Separator<sup>u</sup>: 5 layers at 0.004" per layer
Case served as cathode collector. Electrolyte: 34 Wt. % KSCN<sup>nn</sup>, except B-56)
Central finned anode (10 fins<sup>q</sup>), AZ31B Mg sheet.

Cell No. B-	53	54	55	56			
Major Variables	Increased acetylene black.	HgSO₄: 10g/9.5%	HgSO <sub>4</sub> : 106g/47%	HgSO <sub>4</sub> : 53g/47% (~63°C) 25 Wt.%KSCN			
Hours to End Voltage (1.5/1.3V)	52/59	101/113	59/72	68/76			
Cathode: Sulfur kk (g/%)	65/40	48/45	20/9	10/9			
Carbon (g/%)	65/40	38/36	90/40	45/40			
Acetylene Black $(g/\%)$	32/20	10/9.5	10/4	5/4			
Total Weight (grams)	162	106	226	113			
Cathode Thickness (inches)	0.30	0.30	0.30	0.30			
Cathode Length (inches)	13.5	6.75	13.5	6.75			
Anode: Apparent Area (cm²)	342	171	342	171			
Electrolyte Volume (cc)	650	425	660	625			
Net Cell Volume (inches <sup>3</sup> )	55	28	55	28			
Load <sup>a</sup> (ohms)	2.7/13.5	5.4/27	2.7/13.5	5.4/27			
Initial Closed Circuit Voltage	1.98	2.09	2.15	2.20			
Peak Closed Circuit Voltage C	1.98	2.12	2.17	2. 25			
End Voltage (heavy load)	1.30	1.30	1.30	1.30			
End Voltage (light load)	1.78	1.77	1.56	1.43			
Peak Current Density (mA/cm <sup>2</sup> ) <sup>d, e</sup>	1.90	2.09	2. 21	2.32			
Observed Coulombs/g Sulfur	563	631*	372*	406*			
Observed F/mol Sulfur	0.19	0.25*	0.50*	0.54*			
Watt Hours/inches Net Cell	0.30	0.62	0.42	0.45			
Terminal O. C. V. (at hours/V)	118/1.99	120/1.92	89/1.91	90/1.33			
No. of Hose Clamps	14	4	18	8			
	Copper Exmet sleeve between case and clamps		Copper Exmet sleeve between case and clamps.				

Double lead wires from cells to loads used on Cells B-49 to B-56, except B-54.

<sup>\*</sup> Based on total oxidants.

and B-60 and -61)

Copper Exmet sleeve between case and clamps.

57	58	59	60	61	62
Electrolyte saturated with HgSO <sub>4</sub> <sup>j</sup>	HgSO <sub>4</sub> j: 10g/9.5%	$HgSO_4^{j}$ : 20g/9.5% Full size	HgSO <sub>4</sub> <sup>j</sup> : 10g/9.5% -40°C	HgSO <sub>4</sub> <sup>j</sup> : 10g/9.5% -63°C	HasO <sub>4</sub> j in Wabril capsule in anode space.
64/84	96/106	95/111	97/127	158/176	71/82
48/50	48/45	96/45.2	48/45.2	48/45.2	48/50
38/40	38/36	77/36.3	38.5/36.3	38.5/36.3	38.5/40
10/10	10/9.5	19/9.0	9.5/9.0	9.5/9.0	9.5/10
96	106	212	106	106	96
0.30	0.30	0.30	0.30	0.30	0.30
6.75	6.75	13.5	6.75	6.75	6.75
171	171	342	171	171	171
425	425	740	620	560	450
28	28	55	28	28	28
5.4/27	5.4/27	2.7/13.5	5.4/27	5.4/27	5.4/27
1.99	2.12	2.06	2.17	2. 20	1.95
1.99	2.13	2.09	2.19	2. 22	1.95
1.30	1.30	1.30	1.30	1.30	1.30
1.81	1.80	1.79	1.90	1.78	1.76
1.92	2.17	2. 10	2. 26	2. 26	1.92
546	592*	615*	724*	1010*	526
0.18	0.23*	0.24*	0.28*	0.40*	0.17
0.43	0.58	0.61	0.73	1.02	0.41
119/2.01	119/1.96	140/2.07	140/2.00	188/1.88	116/2.02
8	8	21	9	8	8

## TABLE II

## ELECTROCHEMICAL CELL TESTS - BOBBIN CONFIGURATION

## Task III - "Mockup" Cells in full hardware

Nominal Discharge Temp.: -73°C Case served as cathode collector.

M-1365 Separator<sup>u</sup>: 5 layers at 0.004" per layer. Electrolyte: 34 Wt. % KSCN nn

Central finned anode (10 fins q), AZ31B Mg Sheet.

Refer to Drawings: B-1227, B-1228, A-1238, and A-1239, Appendix B

Refer to Parts and Materials List, Appendix B

Cell No. B-	63	64						
Major Variables	HgSO₄ <sup>j</sup> 20g/9.5%	HgSO <sub>4</sub> <sup>j</sup> 20g/9.5%						
Hours to End Voltage (1.5/1.3V)	81/101	87 / 97						
Cathode: Sulfur kk (g/%)	96/45.2	96/45.2						
Carbon (g/%)	77/36.3	77/36.3						
Acetylene Black (g/%)	19/9.0	19/9.0						
Total Weight (grams)	212	212						
Cathode Thickness (inches)	0.30	0.30						
Cathode Length (inches)	13.5	13.5						
Anode: <sup>q</sup> Apparent Area (cm²)	342	342						
Electrolyte Volume (cc)	500	500						
Net Cell Volume (inches <sup>3</sup> )	39	39						
Load <sup>a</sup> (ohms)	2.7/13.5	2.7/13.5						
Initial Closed Circuit Voltage	2.15	2.18						
Peak Closed Circuit Voltage	2.18	2.19						
End Voltage (heavy load)	1.50	1.50						
End Voltage (light load)	1.99	1.97	<del></del>					
Peak Current Density (mA/cm <sup>2</sup> ) <sup>d, e</sup>	2.17	2.21	2.21					
Observed Coulombs/g Total Oxidants	486	521	521					
Observed F/mol Total Oxidants	0.19	0.20						
Watt Hours/inches <sup>3</sup> Net Cell	0.74	0.79						
Terminal O. C. V. (at hours/V)	112/2.10	113/2.15						
No. of Hose Clamps	7	7	<del></del>					

No copper Exmet; double lead wires

## TABLE III-A (Prismatic Cells)

Test No.	High	Load	Volta	9. 41	after: (hours)	$\frac{72}{2}$	$\frac{12}{12}$	Load V 24	Voltage	after 48	after: (hours) 48 60 72	rs) 72	Hours 1.5V	to: d
P-54 P-56	1.74	1.33	0.85 1.43	0.98	! !		2.15	2.02 1.93	1.70 1.66	1.17	; ;	; ;	20 34	30 40
P-58 P-59 P-60	1.68 2.06 2.08	1.65 1.85 2.04	1.59 1.12 1.86	1.58 .93 1.52	1.46	1.38	1.97 2.24 2.24	1.94 2.12 2.23	1.92 2.12 2.20	1.91	1.88	1 . 84	53 24 55	89 26 56
P-61 P-62 P-63	1.90 1.65 2.05	1.90 1.57 2.12	1.89 1.56 1.60	1.58 1.43 1.55	1.69 1.28 1.30	1.51	1.95 2.01 2.17	1.94 1.97 2.20	1.95 1.95 1.80	1.84 1.89 1.73	1.88 1.81 1.75	1.80	73 40 54	83 60 66
P-65 P-66 P-69	2.15 2.14 1.57	1.95 2.15 1.54	1.60 1.95 1.60	1.27 1.62 1.54	1.62	1.50	2. 22 2. 23 2. 00	2.17 2.23 2.02	1.80 2.17 2.10	1.53 1.88 2.09	1.88	2.10	42 67 81	57 69 202
P-70 P-71 P-72	1.55 1.80 1.72	1.53 .70 1.06	1 . 55	1.51	1.45	1.40	1.90 1.90 2.22	1.89 1.54 1.85	1.89	1.85	1.84	1.82	54 13 17	85 13 20
P-74 P-75	1.33	1.30	1.26 1.35	1.32	1.30	: : : :	1. <b>8</b> 1 1.79	1.75	1.76	1.77	1.77	1 1 1 1 1 1	4 0	27 56
P-76 P-77	1.80	1.80	1.76	1.76	1.68 1.68	1.68	1.98	2.00	1.98	1.98 1.99	1.96 1.96	1.95 1.95	99	141 120
P-78 P-79 P-80	1.82 1.90 1.70	1.85 1.82 1.62	1.81 1.80 1.50	1.81 1.78 1.28	1.70	1.71	2.00 2.00 1.95	2.02 2.00 1.94	2.00 1.99 1.90	2.01 1.99 1.81	1.98 1.97 1.78	1.95 1.95 1.72	93 94 36	103 106 47

TABLE III-A (Prismatic Cells)

s to: 1.3V	118	121	87	108	89	109	100		72	85	80	98	58	28	55	105	81	75	20	54	22		49	
Hour 1.5V	85	82	80	83	75	72	89	45	44	92	25	81	42	54	43	73	29	51	42	44	99	38		46
urs) 72	5.06	2.03	1.97	2.02	1.88	1.85	1.80	1.70	1.85	1.90	1.92		1 1	!	: !	1.93	1.86	1.68	!!	1 1	1.65	1 1	!	1.65
r: (ho	0	2.05	2.00	2.09	1.92	1.90	1.84	1.76	1.85	1.90	1.93	1.92	1.78	1.80	1.61	2.01	1.90	1.76	!	1 1	1.82	!	1 1 ,	1.71
e afte	2.00	1.97	1.98	2.07	1.94	1.92	1.88	1.79	1.87	1.92	1.92		1.83	1.95	1.89	2.06	1.97	1.87	1.68	1.69	1.97	1.67	1.80	1.81
Voltage after: (hours 36 48 60 73	1.99	1.97	2.00	2.08	1.95	1.94	1.90	1.82	1.88	1.92	1.93	1.94	1.90	1.98	1.93	2.04	1.96	1.92	1.84	1.76	2.00	1.78	1.73	1.90
Load 24	1.99	1.98		2.07	2.00	1.97	1.95	1.89	1.90	1.93	1.95	1.95	1.95	2.02	2.01	2.04	2.00	•	1.92	1.83	2.03	1.87	1.89	1.98
Low 12	1.99	2.00	2.02	2.05	2.01	1.99	1.96	1.94	1.93	1.95	1.95	1.95	1.97	2.00	2.00	2.01	1.99	0.	1.98	00	2.05	1.90	1.90	1.97
rs) 72	1.81	1.78	1.70	1.80	1.52	1.48	1.45	1.21	1.29	1.53	1.47	1.60	!	!	; ;	1.50	1.45	1.34	1 1	1 1	1.35	1 1	1 6	1.32
after: (hours	1.85	1.84	1.80	1.93	1.60	1.58	1.51	1.35	1.35	1.55	1.46	1.52	1.24	1.19	1 1	1.68	1.57		1	:	1.55	1 1 1	1 1	1.38
e after	1.81	1.74	1.77	1.87	1.63	1.57	1.56	1.45	1.46	1.60	1.51	1.60	1.40	1.58	1.44	1.81	1.73	1.55	1.35	1.44	1.74	1.29	1.32	
Voltag		1.77	1.83	1.91	1.65			1.52		1.63	1.60	1.62	1.56	1.72	1.57	1.81	1.75	1.67	1.60	1.57	∞.	1.52	1.46	1.65
Load Volta	1.81	٠.7	1,85		1.75		9.	1.60	.5	1.65	1.67	1.68	1.65	1.81	. 7	1.85		. 7		9.	1.88			1.79
High 12	1.82		1.86	1.87	1.77	1.79		1.65		1.68	1.70	1.70	1.73	1.80	1.79	1.85	•	∞.		1.81	6		∞.	1.85
Test No.	<b>P-</b> 81	P- 82	P- 83	P- 84	<b>P-</b> 85	P- 86	P- 87	1	P- 89	P- 90	<b>P-</b> 91	<b>P-</b> 92	P- 93	ı	P- 95	P- 96	. 1	P- 99	P-100	-	10	P-103	-10	-10

TABLE III-A (Prismatic Cells)

12	Test	High	Load	Volta	ge afte	er: (ho	urs)	Low	Load	Voltag	e afte	r: (hou	ırs)	Hours	to:
65         1.62         1.56         1.40         1.17          1.71         1.72         1.70         1.73         1.70         1.73         1.70         1.73         1.70         1.73         1.70         1.71         1.66         1.66         1.66         1.66         1.66         1.66         1.66         1.66         1.70         1.71         1.66         1.66         1.70         1.71         1.66         1.66         1.71         1.66         1.66         1.73         1.70         1.71         1.66         1.71         1.66         1.71         1.66         1.71         1.66         1.71         1.72         1.73         1.74         1.73         1.73         1.74         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.73         1.		12	21	36	48	09	72	12		36	48	9	72	1.5V	$\frac{1.3V}{}$
52         1.40         1.33           1.87         1.82         1.77         1.78           95         1.85         1.77         1.78          91         1.95         1.85         1.77         1.78          91         1.95         1.85         1.77         1.78          91         1.95         1.85         1.77         1.78          91         1.95         1.85         1.77         1.78          91         1.95         1.85         1.93          92         1.95         1.95         1.93         1.9		9.	9.		1.40	1.17	! !	1.71	1:72 1.73	1.70	1.70 $1.71$	1.63	!!!	42	54 56
1.90       1.89       1.85       1.75       1.59       1.32¹       2.07       2.06       2.06       2.02       1.95         2.03       1.93       1.58       1.33        2.12       2.06       1.91       1.79          2.01       1.85       1.42       1.20        2.10       2.03       1.80       1.20          1.23       .70         2.10       2.03       1.80       1.20          1.73       1.62       1.25         2.00       1.78       1.55           1.73       1.62       1.25         2.02       1.96       1.58           1.75       1.86       1.35         2.02       1.96       1.58           2.18       1.98       1.43         2.23       2.10       1.57         2.23       2.10       1.57          2.23       2.09       1.61       1.83       1.83       1.83       1.83       1.83       1.83       1.83 <td></td> <td>7.00</td> <td>4. c. c.</td> <td>6.60</td> <td>7</td> <td>1.54</td> <td>1.33</td> <td></td> <td></td> <td>7 0</td> <td>- 60</td> <td>1.93</td> <td> 1.62<sup>1</sup></td> <td>15 13 64<sup>1</sup></td> <td>44 37 75<sup>1</sup></td>		7.00	4. c. c.	6.60	7	1.54	1.33			7 0	- 60	1.93	 1.62 <sup>1</sup>	15 13 64 <sup>1</sup>	44 37 75 <sup>1</sup>
1.23       .70          2.00       1.78       1.55   2.23       2.10       1.57         2.29       2.09       1.61       1.52          2.29       2.09       1.61       1.52          2.29       2.09       1.61       1.52          2.29       2.09       1.61       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83		0 0	œ. σ. ∞.	α·. 4.	1.75 1.33 1.20	1.59	1.321	0		2.06 1.91 1.80	0 2	1.95	1.791	65 <sup>1</sup> 38 34	73 <sup>1</sup> 52 39
2.18       1.98       1.43         2.29       2.10       1.57  1.45       1.45       1.43       1.86       1.80       1.80       1.82       1.82       1.82       1.82       1.82       1.82       1.82       1.82       1.82       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.83       1.84		2 7 6	. 6 . 8	.3		[		1.45 2.00 2.02	. 92 1. 78 1. 96			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	! ! !	8 30 32	11 35 38
2.17       1.93       1.70       1.03         2.23       2.02       1.91       1.18                                  1.85       1.85       1.80       1.83       1.82       1.87       1.87       1.87       1.87       1.87       1.81       1.         1.70       1.63       1.54       1.46       1.35       2.00       1.98       1.94       1.87       1.81       1.         1.74       1.67       1.61       1.55       1.46       1.40       2.03       2.00       1.98       1.92       1.87       1.         1.27       1.24          1.65       1.65       1.65	<b>^ ^ -</b>	7 2 7	6.6.8	4 4 m	1 . 1	1 1 i 1 1 i 1 i 1	1 1 1			1.57 1.61 1.45	. 5	; ; ; ; ; ; ; ; ;		35 35 29	39 51 38
1.51       1.50       1.45       1.45       1.42       1.88       1.88       1.90       1.80       1.83       1         1.49       1.59       1.58       1.57       1.53       1.85       1.88       1.87       1.87       1       1         1.85       1.56       1.20         1.90       1.75       1.35  -	10 .0 6	149		γ 4	1.03 1.48 1.45	1.45	1.43	2 00 00	$\circ$	1.91 1.80 1.80		1.83 1.82	1.80	41 0 12	43 95 89
1.70 1.63 1.54 1.48 1.40 1.35 2.00 1.98 1.94 1.87 1.81 1. 1.74 1.67 1.61 1.55 1.46 1.40 2.03 2.00 1.98 1.92 1.87 1. 1.27 1.24 1.65 1.65	~ ~ ~	24.00	$\alpha$		40	1.45	4.70 1	1.88 1.85 1.90	1.88 1.88 1.75	1.90 1.87 1.35	∞ ∞ ı	$\infty \infty $ 1	1.81 1.86	25 90 25	110 113 30
		. 7	9.00	1 . 6	1	1.40	ε 4 -	0 0		661		1.81		45 57 0	82 83 <12

<sup>1</sup> Recorder failure; voltage estimated.

TABLE III-B (Bobbin Cells)

s to:	28 31 35	70 42 <sup>2</sup> 21	18 26 56	22 62 42	63 91	30	73 84 51
Hours to:	22 20 31	50 18 10	1 19 23	0 54 25	36 80	26 59	66 71 51
rrs)					1.85	! !	1.79
Load Voltage after: (hours)  24 36 48 60 72		1.85	1.77	1.84	1.85 1.86	; ; ! !	1.90 1.90 1.75
e afte	! ! !	1.89 1.68 1.75	1.70	1.92	1.86 1.85		1.91 1.91 1.89
Voltag	1.85	1.95 1.66 1.69	1.75 1.81	1.63 1.93 1.87	1.87	1.52	1.92 1.93 1.91
	1.92 1.93 2.01	1.96 1.66 1.65	1.51 1.70 1.76	1.68 1.82 1.85	1.86	1.98	1.91 1.94 1.91
Low 12	1.99 1.97 2.04	2.00 1.75 1.78	1.65 1.89 1.82	1.77 1.93 1.85	1.87	2.11	1.93 1.88 1.94
rs)	; ; ;				1.52	(at -40°C) (at -63°C)	1.30
after: (hours)	: : :	1.35	1.20	1.33	1.33	(at -	1.60 1.55 1.25
a) T	1 1 1	1.51 1.28 <sup>2</sup> 1.31	1.50 1.40	1.53	1.40	1.10	1.66 1.53 1.56
High Load Voltagon $\frac{12}{1}$ $\frac{24}{2}$ $\frac{36}{3}$	1.19 1.25	1.58 1.32 1.26	1.40 1.47	1.06 1.60 1.40	1.49	1.26	1.69 1.60 1.61
Load 24	1.40 1.40 1.65	1.62 1.37 1.21	. 95 1. 31 1. 46	1.20 1.56 1.55	1.52	1.60	1.67 1.55 1.58
High	1.63 1.59 1.78	1.71 1.52 1.45	1.33 1.63 1.50	1.35 1.65 1.50	1.52	1.92	1.69 1.57 1.65
Test No.	B- 4 B- 6	B- 7 B- 8 B- 9	B-10 B-12 B-13	B-14 B-15 B-16	B-17 B-19	B-22 B-22	B-23 B-24 B-25

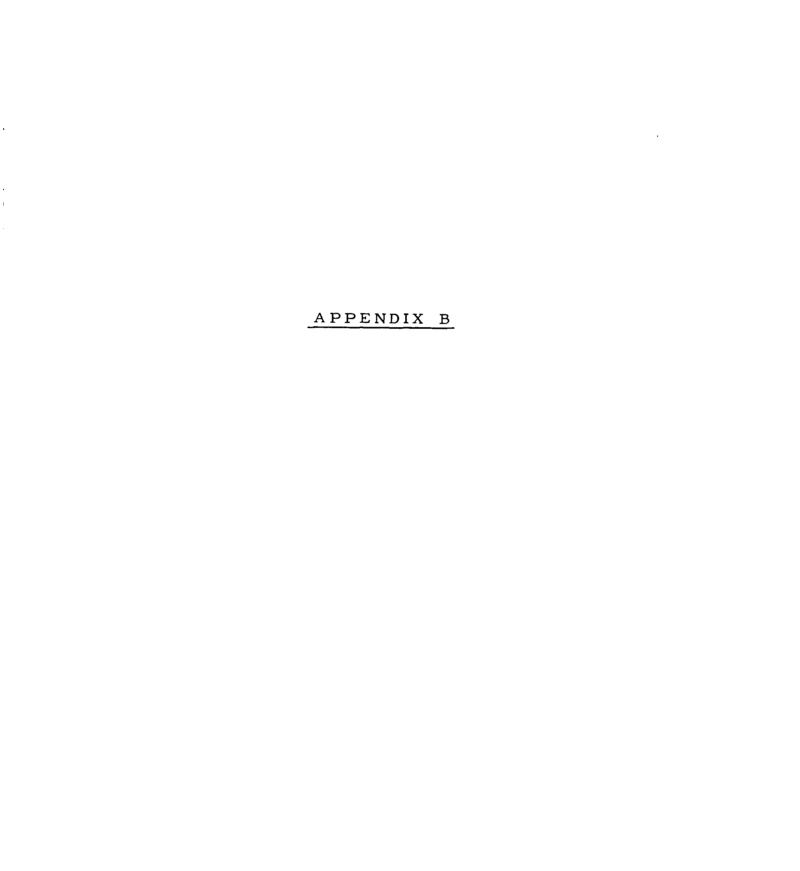
<sup>2</sup> Temperature increase; voltage estimated.

TABLE III-B (Bobbin Cells)

s to:	67 47 57	41 76 53	75 63 70	53 56	63 73 61	100 108 61	77 58 65	58 63 116
Hours 1.5V	56 40 53	30 68 43	67 56 61	48 51	54 59 47	83 99 49	55 52 57	52 55 67
urs) 72	1.62	1.83	1.81	       	1.83	2.05 2.05	1.84	1.86
r: (ho	1.76	1.88	1.89 1.85 1.86	1.70	1.83 1.90 1.60	2.05 2.05 1.80	1.85 1.77 1.83	1.75 1.80 1.91
ge afte	1.85 1.81 1.90	1.73 1.90 1.85	1.92 1.90 1.90	1.86 1.86	1.88 1.88 1.71	2.08 2.07 1.85	1.90 1.87 1.86	1.86 1.84 2.05
Voltage after: (hours) 36 48 60 72	1.88 1.91 1.90	1.87 1.91 1.95	1.95 1.93 1.94	1.95	1.94 1.93 1.81	2.07 2.08 1.90	1.92 1.91 1.90	1.90 1.89 2.05
Load	1.90 1.93 1.91	1.95 1.92 1.98	1.95 1.95 1.97	1.94	1.94 1.95 1.89	2.09 2.09 1.92	1.91 1.95 1.92	1.92 1.90 1.95
Low 12	1.93 1.91 1.92	1.96 1.91 1.96	1.97 1.96 1.97	1.95	1.95 2.08 1.97	2.13 2.12 1.95	1.95 1.97 1.95	1.95 1.94 1.96
rs)	1.16	1.38	1.35	1 1	1.30	1.66	1.38	1.47
after: (hours)	1.43	1.61	1.59 1.36 1.52	1.12	1.35 1.49 1.35	1.70 1.74 1.33	1.45 1.25 1.44	1.24 1.43 1.64
e after	1.59 1.25 1.58	1.15 1.67 1.36	1.64 1.60 1.67	1.48 1.55	1.56 1.56 1.43	1.83 1.80 1.54	1.62 1.55 1.58	1.54 1.54 1.81
Voltag 36	1.65 1.56 1.66	1.42 1.70 1.60	1.67 1.65 1.75	1.72 1.70	1.70 1.71 1.65	1.85 1.86 1.67	1.70 1.63 1.65	1.65 1.65 1.88
High Load Voltag	1.65 1.59 1.67	1.59 1.70 1.67	1.67 1.66 1.72	1.66 1.64	1.66 1.76 1.72	1.93 1.94 1.69	1.70 1.64 1.67	1.70 1.67 1.72
High 12	1.66 1.56 1.69	1.60 1.70 1.65	1.70 1.70 1.72	1.70	1.72 1.85 1.81	2.00 1.98 1.70	1.74 1.69 1.66	1.70 1.70 1.72
Test No.	B-26 B-27 B-28	B-29 B-30 B-31	B-32 B-33 B-34	B-35 B-36	B-37 B-38 B-39	B-40 B-41 B-42	B-43 B-44 B-45	B-46 B-47 B-48

TABLE III-B (Bobbin Cells)

High	Load	High Load Voltage		after: (hours)	ırs)	Low		Load Voltage After: (hours)	ge Afte	r: (ho	urs)	Hon	Hours to:
	24	36	48	9	72	15	24	<del>36</del>	48	09	72	1.50	1.30
96	1.95	1.70	1.47	1.39	1.40	2.10	2.10	1.91	1.85	1.83	1.85	47	127
92	1.78	1.75	1.62	1.36	1 1	1.95	1.95	1.91	1.85	1.82	!	99	61
74	1.74	1.74	1.67	1.57	1.23	1.92	1.91	1.91	1.88	1.86	1.76	62	69
71	1.73	1.70	1.63	1.50	1.22	1.93	1.91	1.90	1.88	1.85	1.80	61	89
1.73	1.74	1.71	1.58	1.29	;	1.93	1.92	1.90	1.85	1.77	1  - 	52	29
87	1.64	1.64	1.61	1.65	1.60	2.10	1.89	1.87	1.85	1.89	1.86	101	113
26	1.96	1.88	2.03	1.46	1.26	2.17		2.15	2.17	1.85	1.56	59	72
14	2.10	2.05		1.80	1.37	2.22	2.20	2.17	2.05	1.94	1.51	89	92
1 76	1 74	1 74	1, 72	1.55	1.37	1.95	1.93	1.92	1.92	1.87	1.82	64	84
93	1.66	1.70	. ~	1.71	1.69	2.12	1.92		1.92	1.91	1.90	96	106
1 92	1 71	1.72	1.68	1.67	1.64	2.10	1.90	1.87	1.88	1.87	1.87	96	111
05	1.97	1.80	1.82	1.81	1.69	2.13	2.11	2.11	2.09	2.07	2.08	26	127
7 05	1 98	1,97	1.95	1.95	1.88	2.20	2.11	2.12	2.10	2.10	2.08	158	176
92	1.75	1.73		1.60	1.45	1.95	1.95	1.92	1.90	1.88	1.84	71	82
44	1 87	1.85	1.84	1.73	1.65	2.08			2.07	2.05	2.03	81	101
1.85	1.89	1.89	1.87	1.80	1.74	2.05	2.08	2.08	2.07	5.06	2.05	87	26



## l. Prismatic Cell Construction

Figure 1 illustrates a prismatic cell comprising a pasted-plate cathode enclosed and sealed within a separator, two magnesium anodes and a plastic envelope case. A silver-plated copper Exmet (expanded metal) grid serves as the carrier for the paste and as a cathode collector. The lead wire is soldered to the Exmet, and the joint is coated with Krylon or rubber cement.

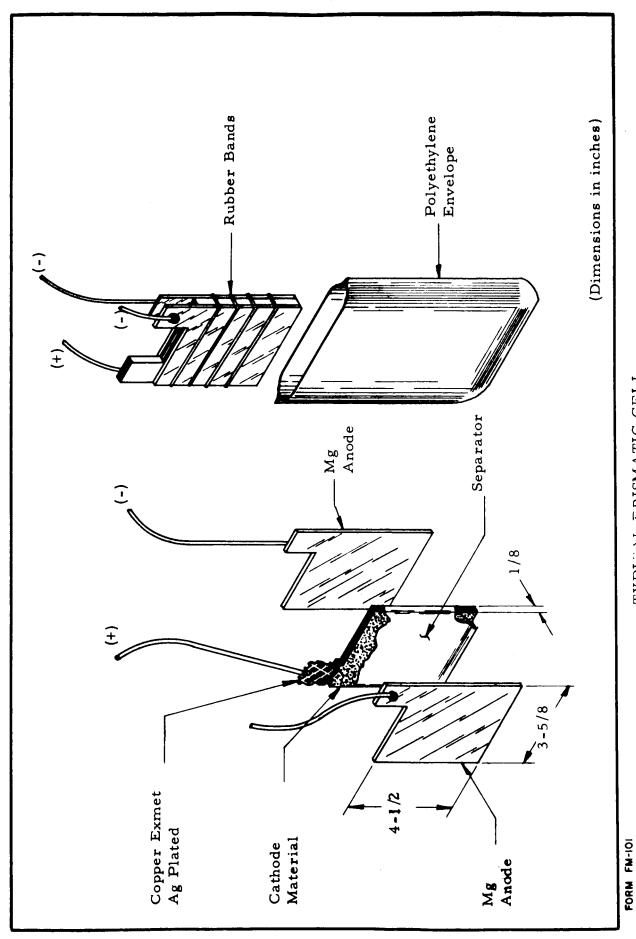
The oxidant(s) and graphite in the desired proportions are dry blended and are then mixed with a binder (1% solution of polystyrene in toluene) into a workable paste. The paste is spread evenly on both sides of the grid with a spatula. During this procedure, the surface may be moistened with toluene as necessary to counteract evaporation. The finished plate is air-dried overnight, or until the odor of toluene has disappeared. Forced drying is not applied in order to avoid shrinking and cracking of the paste.

A suitable separator is then wrapped around the dried plate and sealed at the seams.

A magnesium sheet anode is applied to each face of the cathode on the outside of the separator, and the two anodes are held in place with rubber bands which permit swelling of the cathode during activation and discharge. The anode lead wires are attached with aluminum rivets, and the connections are protected with Krylon or rubber cement.

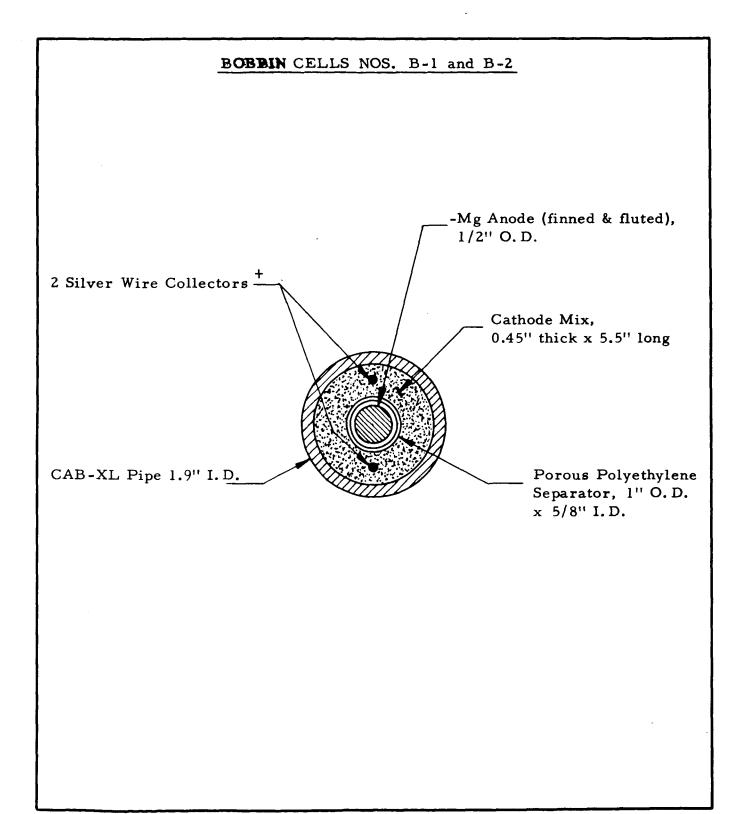
The entire cell assembly is encased in a polyethylene envelope which may be used for discharge at any temperature below the boiling point of liquid ammonia.

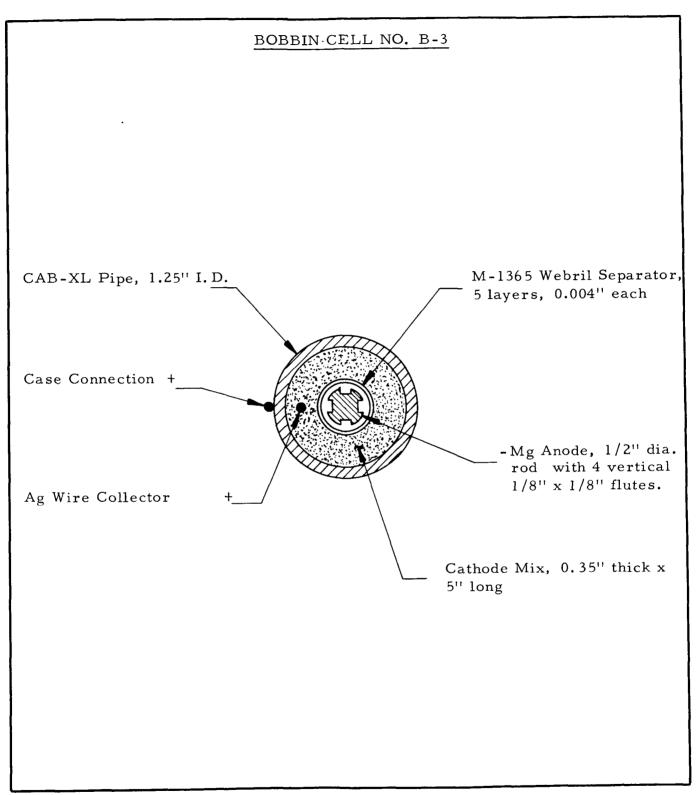
The general design may be varied at will to meet the requirements of special tests.



TYPICAL FRISMATIC CELL

Figure 1





FORM FM-100

Figure 3

## BOBBIN CELL NO. B-4

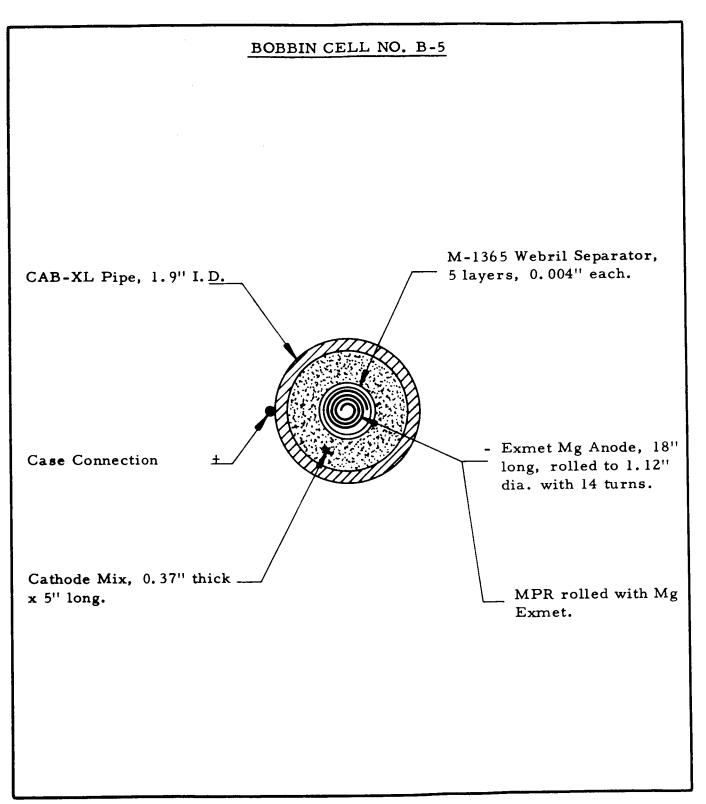
Case Connection

Exmet Mg wrapped with 5 layers of M-1365 Webril, 0.004" each.

- Exmet Mg Anode, 18" long, rolled to 13/16" dia. cylinder.

Cathode Mix, 0.32" thick x 6" long.

FORM FM-100



FORM FM-100

Figure 5

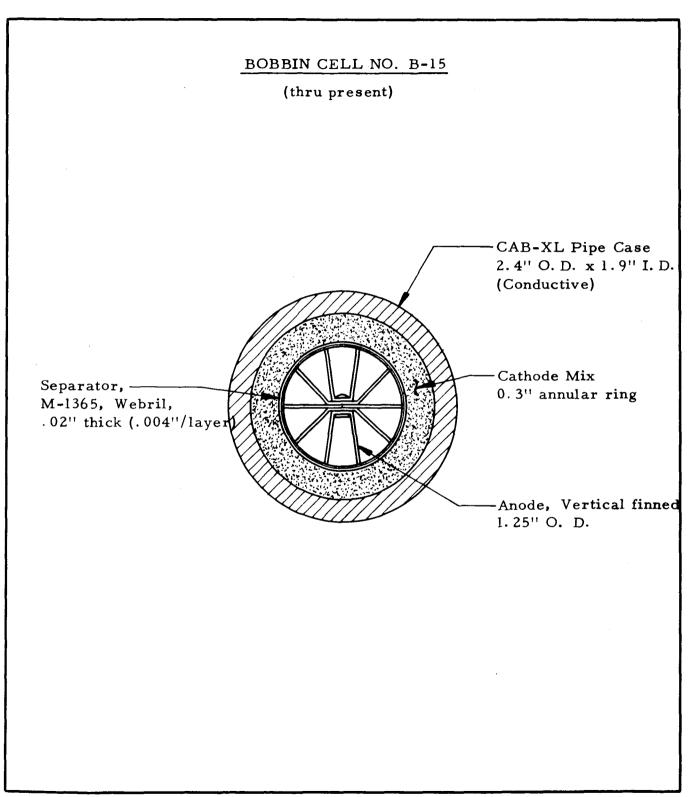
## BOBBIN CELL NO. B-6 M-1365 Webril Separator, 5 layers, 0.004" each. CAB-XL Pipe, 1.9" L.D. Case Connection Exmet Mg Anode, 42" long, rolled to cylinder 1.31" dia., with 20 turns. Cathode Mix, 0.27" thick x 5" long.

FORM FM-100

## BOBBIN CELL NO. B-7 + Ag Wire Collector (4) CAB-XL Pipe, 1.9" I.D. Mg Exmet Anode, M-1365 Webril Separator 5-3/8" circumference 5 layers, 0.004" each. with 20 1/4" dia. holes Cathode Mix, 0.24" Mg Exmet Anode, thick x 5.25" long 5-1/8" circumference with 20 1/4" dia. holes Mg Exmet Anode, - Mg Exmet Anode, 8-7/8" 4-15/16" circumference long, rolled in 3 turns to an with 20 1/4" dia. holes O.D. of 1.01", with 20 1/4" dia. holes.

FORM FM-100

Figure 7



FORM FM-100

## 2. BOBBIN CELL CONSTRUCTION

A variety of designs were tried in the early stages until one suitable for most of the experimental work of Task I was devised. Upon completion of the first task, "Task II, Design" was carried to conclusion. In this, a self-contained ammonia cell in full hardware, excluding activator, was designed.

## 2.1. Task I, Experimental Cells

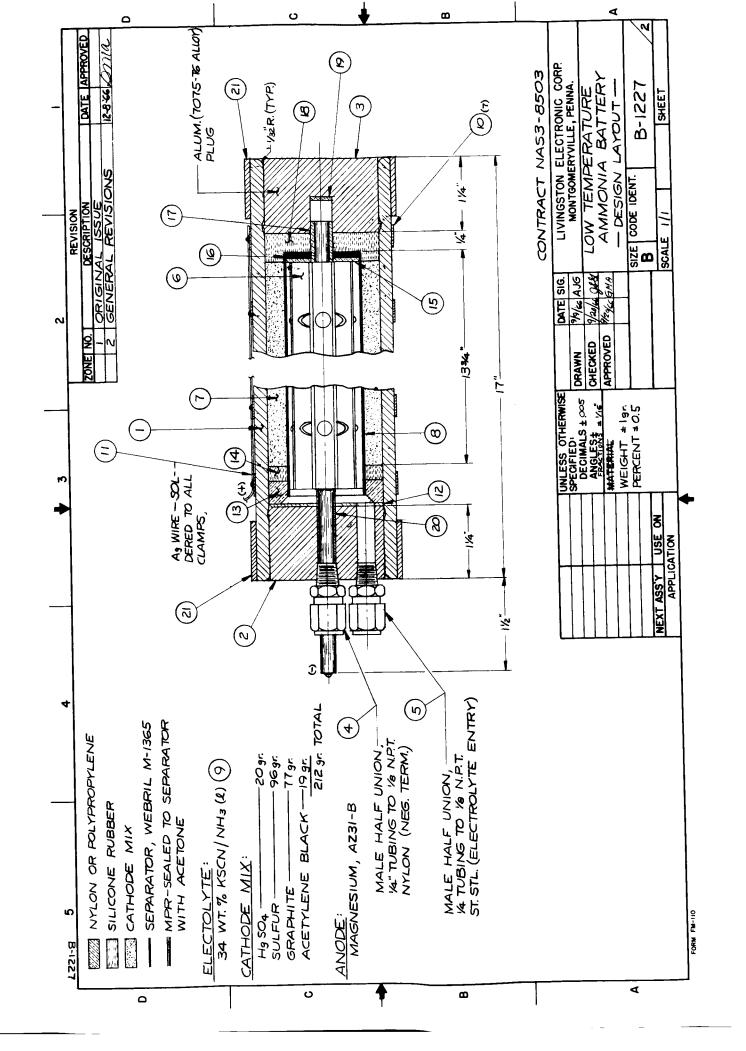
All of these cells had open tops. Some were full-length; some, half-length. The cell assembly is shown in Figure 9, page 43; the anode design, in Figure 10, page 44; and a cross-sectional view, in Figure 8 of Appendix B, page B-9. The construction steps follow in sequence:

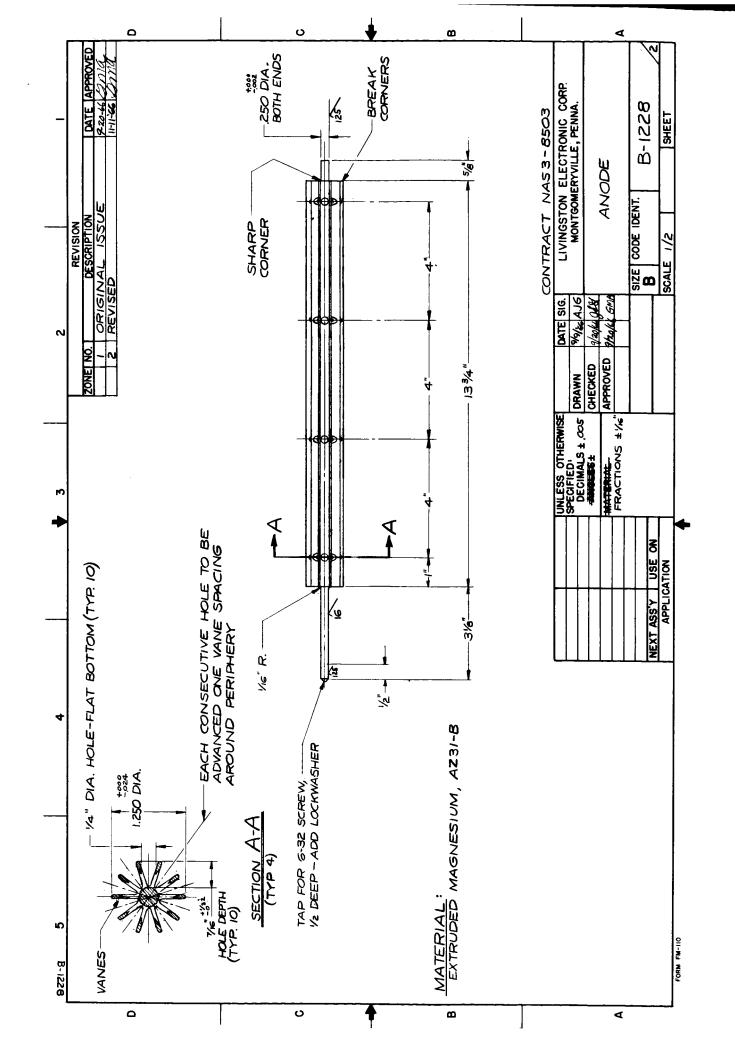
- 1. Five (5) layers of M-1365 Webril separator paper are wrapped around a 1-1/4 inch diameter mandrel. The paper is folded over at the bottom to form a cylindrical cup, and all seams are sealed with acetone.
- 2. The anode is fabricated as shown in Figure 10, page 44.
- 3. A metal plug is pressed into a bottom of the plastic case.
- 4. The separator cup with mandrel in place is placed in the center of the case, and the cathode mixture is packed between the separator and the wall of the case in ten increments with a piston which fits the annular space. Each increment is packed to occupy 1/10 of the total cathode depth.
- 5. The mandrel is then removed from the separator cup and is replaced by the anode with its negative connection.
- 6. The positive connection is made by soldering a wire to several adjustable bands attached to the outside of the conductive plastic case. Seven clamps are used on full-sized cells; four, on the half-sized ones.

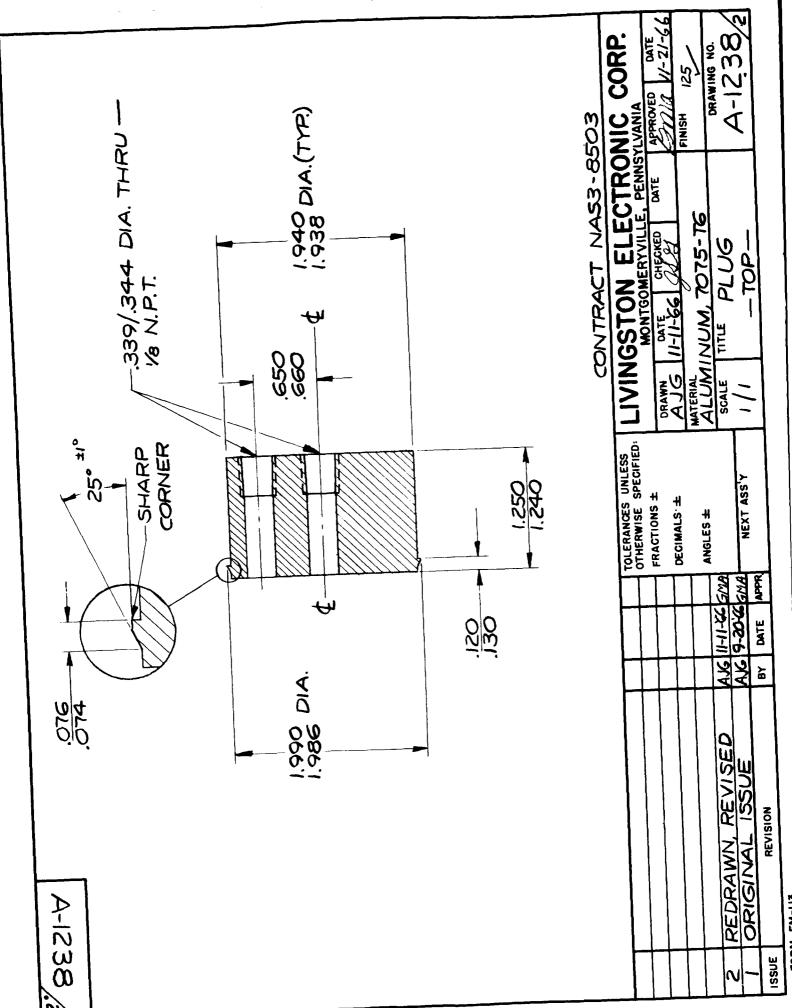
## 2.2. Task II, Design

This cell, a refined version of the experimental cell with a top as well as a bottom closure, is detailed in drawings B-1227, B-1228, A-1238, and A-1239 which are supplemented with a Parts and Materials List. These illustrations follow this construction procedure. The parts numbers will be shown in parentheses where appropriate. After all parts have been made, they are assembled in the following sequence:

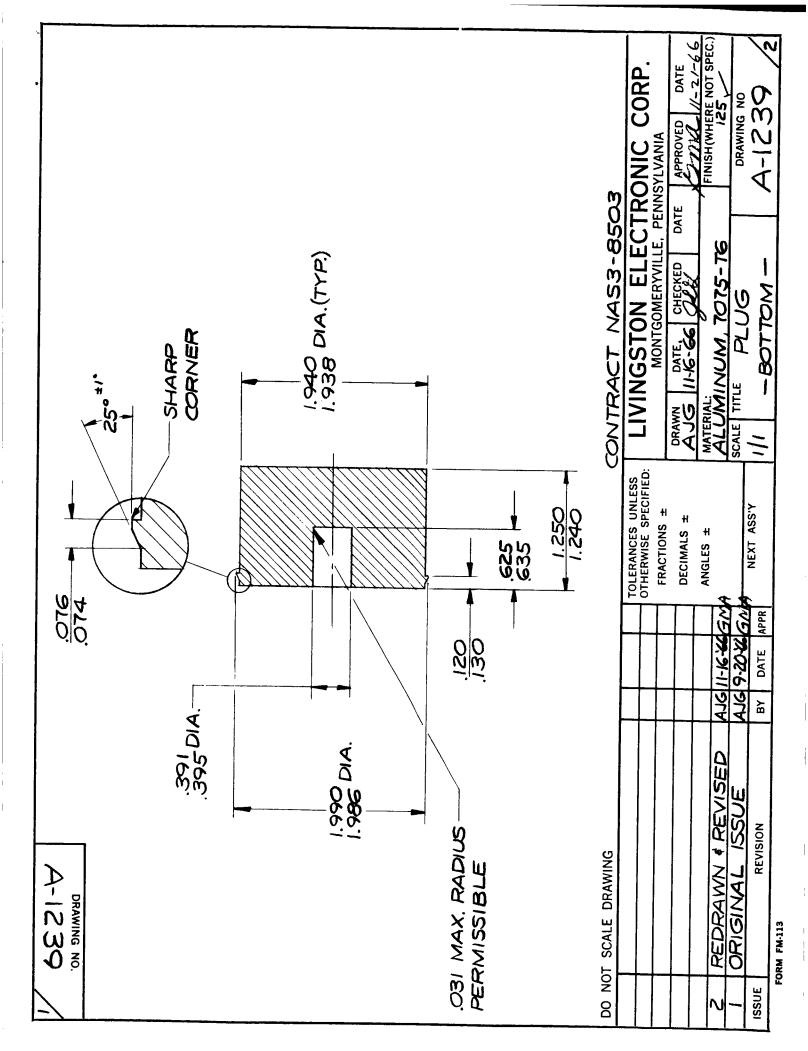
- 1. The bottom metal plug (3) (silicone primed) is pressed into position in the plastic case (1), and disc (19) is inserted.
- 2. The hole in the bottom plug is stoppered, and then a silicone encapsulant (18) is poured onto the plug to a depth of 1/4 inch. After a 16 hour curing period, the stopper is removed.
- 3. Five layers of M-1365 Webril separator paper (8) are wrapped around a l-1/4 inch diameter arbor and sealed with acetone. In the bottom end, a polypropylene disc (15) and a microporous rubber disc (16) are inserted. Then, the separator is folded over at the bottom and sealed, after which a second disc (15) is placed over the end. This separator cup with arbor in place is inserted in the case.
- 4. The cathode mixture (7) is packed between the separator and the case in ten increments with a hollow cylindrical piston. Each increment is packed to occupy 1/10 of the total cathode length.
- 5. The arbor is replaced by the anode (6), the bottom 1/4 inch diameter extension of which is insulated with a nylon sleve (17).
- 6. A 1/4 inch layer of silicone rubber (14) is poured on top of the cathode mix and is allowed to cure.
- 7. This is followed by a polypropylene spacer ring (13).
- 8. The top plug (2), with an insulating disc (12), is pressed into place.
- 9. Hose clamps (10) are then placed on the case and tightened. The end ones help to hold the plugs in place. The others, to which a silver wire (11) has been soldered, serve as current collectors.
- 10. A stainless steel male half union (5) for the electrolyte fill port and a nylon male half union (4) to insulate the extension of the anode from the metal plug and case are then inserted and tightened.
- 11. The finished cell is carefully tested for leaks under pressure. If free from leaks, it is ready for activation.







FORM FM-113



# PARTS AND MATERIALS LIST

Project #652	#652	Prepared By J. S. Gore	Approved By G. M. Armstrong
Contract	Sontract NAS 3-8503	Date September 20, 1966	Date September 20, 1966
bart No.	Req.	Item Description	
1	1	Plastic Pipe - CAB-XL, 2" I. P. S. sch. 80; Cabot Corporation, Louisville, Ky.	
2	-	Top Plug - Aluminum alloy 7075-T6 (Dwg. No. Al 238); Metal Supply Co., Philadelphia,	
3	1	Bottom Plug - Aluminum alloy 7075-T6 (Dwg. No.A1239); Metal Supply Co., Philadelphia,	Supply Co., Philadelphia, Pa.
4	1	Nylon Insulator - Nylon male half union, 1/4" tubing to 1/8" N. P. T.; Crawford Fitting Co., Solon, Ohio	l. P. T.;
Z.	1	Fill Port - Stainless steel male half union, 1/4" tubing to 1/8" N.P.T.; Crawford Fitting Co., Solon, Ohio	" N. P. T.;
9	П	Anode - Extruded magnesium, alloy AZ31-B (Dwg. No.B12%); White Metal Rolling and Stamping Corporation, Brooklyn, N.Y	; clyn, N.Y.
2	1	Cathode - Dry packed powder	
		a. Mercuric sulfate - A.R. Grade; Mallinckrodt Chemical Works, St. Louis, Mo. b. Sulfur - Sublimæd; Matheson Co., Inc., E. Rutherford, N.J. c. Carbon - Air spun graphite, Type 200-44; Joseph Dixon Crucible Co., Jersey City, N.J. d. Carbon - Acetylene black; Shawinigan Products Corp., Englewood Cliffs, N.J.	emical Works, St. Louis, Mo. rford, N.J. h Dixon Crucible Co., Jersey City, N.J. Corp., Englewood Cliffs, N.J.
<sub>∞</sub>	1	Separator - Webril M-1365, acetate-cotton fabric; Kendall Co., Walpole, Mass	o., Walpole, Mass.
6	П	Electrolyte - 34 weight percent KSCN in NH <sub>3</sub> (L)	
		a. KSCN - Reagent B & A Code 2144; Allied Chemical Co., New York, b. $NH_3$ (L) - Anhydrous; National Ammonia, Philadelphia, Pa.	cal Co., New York, N.Y. elphia, Pa.
10	6	Clamps - Stainless steel size #32; Ideal Corporation, Brooklyn, N.Y	л, N.Y.
11	1	Connection - #18 AWG silver wire soldered to 7 clamps; T.B. Hagstoz & Sons, Philadelphia,	. Hagstoz & Sons, Philadelphia, Pa
12	1	Insulator Disc 040" polypropylene drilled for fill port and anode rod; Commercial Plastics and Supply Corporation of Penna.,	anode rod; of Penna., Philadelphia, Pa.

## PARTS AND MATERIALS LIST

ore Approved By G. M. Armstrong	966 Date September 20, 1966	ription	O.D. x 1.300" I.D. x .375" high polypropylene; rcial Plastics and Supply Corporation of Penna., Philadelphia, Pa.	RTV 3110; Dow Corning Corp., Midland, Mich.	.375" I.D.; p. of Penna., Philadelphia, Pa.	n Hard Rubber Co., Butler, N.J.	Nylon 0.375" O.D. x 0.250" I.D. x 0.687" long; Commercial Plastics & Supply Corp. of Penna., Philadelphia, Pa.	Dow Corning Corp., Midland, Mich.	p. of Penna., Philadelphia, Pa.	Polyvinyl chloride 0.250" I. D. x 0.312" O. D. x 1" long; Commercial Plastics and Supply Corp. of Penna., Philadelphia, Pa.
Prepared By J. S. Gore	Date S		O 74	Seal - Silicone rubber RTV 3110; Dow Cornin	Disc040" polypropylene l. 250" O. D. x 0. 375" I. D.; Commercial Plastics and Supply Corp. of Penna.,	Disc040" microporous rubber; American Hard Rubber Co., Butler, N.J.	Insulator Sleeve - Nylon 0.375" O.D. x 0.250" I.D. x 0.687" long; Commercial Plastics & Supply Corp. of Penna.,	Shock Absorber - Silicone rubber RTV 3110; Dow Corning Corp., Midland, Mich	Disc040" polypropylene 0.531" dia.; Commercial Plastics and Supply Corp. of Penna., Philadelphia,	Insulator Sleeve - Polyvinyl chloride 0.250" I. D. $x$ 0.312" O. D. $x$ 1" long; Commercial Plastics and Supply Corp. of Penna., Phila
#652	Contract NAS 3-8503	Req.	<b></b>	-	7	7	-	1	-	П
Project #652	Contrac	Part No.	13	14	15	16	17	18	19	20

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